ULTRAFILTRATION OF BLOOD BETWEEN TWO PARALLEL MEMBRANES

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ULTRAFILTRATION OF BLOOD BETWEEN TWO PARALLEL MEMBRANES

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<th>Symbol</th>
<th>Description</th>
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<tr>
<td>$F$</td>
<td>a function of $\psi$ defined in equation (3-19)</td>
</tr>
<tr>
<td>$F'$</td>
<td>$aF/\partial \psi$</td>
</tr>
<tr>
<td>$g$</td>
<td>gravitational acceleration, cm/sec$^2$</td>
</tr>
<tr>
<td>$h$</td>
<td>grid step size in x-direction, cm</td>
</tr>
<tr>
<td>$H$</td>
<td>half-distance between the two parallel membranes, cm</td>
</tr>
<tr>
<td>$I$</td>
<td>positive integer in x-direction</td>
</tr>
<tr>
<td>$J$</td>
<td>positive integer in y-direction</td>
</tr>
<tr>
<td>$k$</td>
<td>1. grid step size in y-direction, cm. 2. square root of ultimate viscosity coefficient, $(\text{gm/cm-secp})^{\frac{1}{2}}$</td>
</tr>
<tr>
<td>$K$</td>
<td>$k/\rho U_0^2$, dimensionless viscosity coefficient</td>
</tr>
<tr>
<td>$L$</td>
<td>length of the flow channel, cm</td>
</tr>
<tr>
<td>$p$</td>
<td>pressure of fluid, dyne/cm$^2$</td>
</tr>
<tr>
<td>$P_f$</td>
<td>pressure factor defined in equation (A-6), dyne/cm$^3$</td>
</tr>
<tr>
<td>$P$</td>
<td>dimensionless pressure</td>
</tr>
<tr>
<td>$P_f$</td>
<td>dimensionless pressure factor</td>
</tr>
<tr>
<td>$Q_0$</td>
<td>entrance volumetric flow rate, cm$^3$/sec</td>
</tr>
<tr>
<td>$R_x$</td>
<td>entrance Reynolds number, $4U_0 H_0 / k^2$</td>
</tr>
<tr>
<td>$R_y$</td>
<td>wall Reynolds number, $\nu_0 H_0 / k^2$</td>
</tr>
<tr>
<td>$s$</td>
<td>step size ratio, $h/k$</td>
</tr>
<tr>
<td>$T_o$</td>
<td>dimensionless yield stress of fluid</td>
</tr>
<tr>
<td>$T_{yx}$, $T_{xx}$, $T_{yy}$</td>
<td>dimensionless stress components</td>
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\[ U_0 \quad \text{entrance average velocity, cm/sec} \]
\[ v_x \quad \text{velocity component in x-direction, cm/sec} \]
\[ v_y \quad \text{velocity component in y-direction, cm/sec} \]
\[ v_0 \quad \text{wall suction velocity, cm/sec} \]
\[ V_0 \quad \text{dimensionless wall suction velocity} \]
\[ V_x \quad \text{dimensionless velocity component in x-direction} \]
\[ V_y \quad \text{dimensionless velocity component in y-direction} \]
\[ W \quad \text{width of the flow channel, cm} \]
\[ x \quad \text{distance in x-direction, cm} \]
\[ X \quad \text{dimensionless distance in x-direction} \]
\[ y \quad \text{distance in y-direction, cm} \]
\[ Y \quad \text{dimensionless distance in y-direction} \]
\[ \alpha \quad \text{relaxation factor in stream-function equation} \]
\[ \beta \quad \text{relaxation factor in shear-stress equation} \]
\[ \gamma \quad \text{shear-stress correlation factor defined in equation (2-35)} \]
\[ \mu \quad \text{Newtonian viscosity coefficient, g/cm-sec} \]
\[ \rho \quad \text{fluid density, gm/cm}^3 \]
\[ \tau \quad \text{shear stress tensor, dyne/cm}^2 \]
\[ \tau_0 \quad \text{yield stress of fluid, dyne/cm}^2 \]
\[ \tau_{yx}, \tau_{xx}, \tau_{yy} \quad \text{stress components, dyne/cm}^2 \]
\[ \psi \quad \text{dimensionless stream function} \]
\[ \psi' \quad \text{conventional stream function defined in equation (4-1)} \]

**Subscript**

\[ x \quad \text{components in x-direction} \]
\[ y \quad \text{components in y-direction} \]
\[ I \quad \text{positive integer, denotes a grid point at } x = I\Delta x \]
\[ J \quad \text{positive integer, denotes a grid point at } y = J\Delta y \]
SUMMARY

Ultrafiltration of blood between two parallel membranes was studied in this work. The blood was considered as a non-Newtonian fluid with rheological properties that follow the Casson equation. Creeping flow, constant physical properties and constant wall suction rates were assumed.

The system was studied as a two-dimensional Cassonian flow. The well known Casson equation for one-dimensional flow was expanded into multi-dimensional flow form as a function of the second invariant of $\Delta$, the symmetrical rate of deformation tensor. The flow equations were first reduced to dimensionless form. A dimensionless stream function and dimensionless shear stresses were defined and the flow equations were reduced to two equations in terms of these variables. Relations between the shear stress components were developed to reduce the four shear stresses to one shear stress.

The stream function equation and the shear stress equation were then rewritten with finite difference approximations for the derivative terms. A successive relaxation procedure was used to obtain numerical values of the stream function and the shear stress. The stream function equation had to be solved iteratively within each relaxation cycle.

Since there was no similar study or experimental data for comparison, the accuracy of the numerical technique used was checked in limiting cases with the results obtained from analytical solutions. The agreement of the iterative results with the analytical results were excellent.
The half distances between membranes were set at 0.005, 0.01 and 0.05 cm. The blood yield stress was taken to be the normal average value of 0.04 dyne/cm² in most cases but other values were also used to study the effect this yield stress term had on the flow. The entrance Reynolds number covered a range from 0.25 to 25. The wall Reynolds number covered a range from zero to 0.025.

It was found that increasing yield stress values caused an increase in shear stress and pressure drop. With wall suction, the shear stress of the fluid and the pressure drop became smaller than those without wall suction. Larger suction rates resulted in smaller shear stress and less pressure drop.

Some relationships between the variables studied were developed to help predict the flow behavior at other flow conditions from the results of known flow conditions.
CHAPTER I

INTRODUCTION

Artificial Kidneys and the Significance of this Study

It has been reported [1] that about 20% of the up to 50,000 people who die each year from kidney disease are suited to artificial kidney treatment or kidney transplantation. The artificial kidney is capable of postponing death from irreversible kidney failure for a few years of even indefinitely in some cases. The artificial kidney is also used routinely to sustain a patient who is waiting for a suitable donor kidney to become available for transplantation.

Ever since Kolff's [2] pioneering treatment in 1943 of the first uremic patient by means of hemodialysis, use of the artificial kidney has increased steadily for the correction of biochemical abnormalities associated with endogenous or exogenous intoxication. Scribner [3] in 1960 demonstrated a permanent cannulation technique which allowed relatively easy access to the blood stream for connection to the artificial kidney on a regular basis. In the following years, the attention of researchers turned to the task of optimizing and simplifying the equipment to increase its reliability and to reduce capital and operating costs. Especially notable were the engineering improvement efforts of Babb and Grimsrud [4], Esmond [5], Stewart [6] and Oja [7].

Although significant improvements have been made by the above-mentioned investigators, the basic means of mass transfer of all the
present day clinical units is still dialysis, which requires a large quantity of specially formulated dialysate and a precise delivery system to carefully control the flow condition of the dialysate. Regardless of how small and efficient the blood-dialysis fluid transfer unit is made, there still remains the cumbersome delivery system requirements of pumping, conductivity control, heat exchange, pressure control, precise stream mixing and safety. Therefore, the patients are literally immobilized for treatment two or three times a week. A portable or wearable treatment unit which can be moved along by the patient is much desired. The only way to achieve this kind of portability is to eliminate the handling of the large quantity of dialysate. This requires a different concept of an artificial kidney. One such concept is the selective ultrafiltration and returning of water and perhaps some necessary electrolytes back to the blood stream while leaving behind the toxic substances such as urea, creatinine, etc. This process would be more analogous to the function of the living kidney than the dialysis process. Preliminary work toward the development of a blood ultrafiltration unit has been done by a few investigators [8-16] but the recovery of water has not yet been attempted.

Because of the many advantages of the ultrafiltration artificial kidney, it is believed that ultrafiltration will ultimately replace dialysis in artificial kidneys.

Very few theoretical studies can be found in the literature on blood ultrafiltration because it has only recently gained importance. The fact that blood is a non-Newtonian fluid and that blood ultrafiltration processes involve two dimensional flow make the mathematical study of this problem very complicated.
It is the object of this work to pioneer into the task of solving such a blood ultrafiltration problem to obtain the flow patterns and velocity-pressure relations which will assist the design of an ultrafiltration artificial kidney and the prediction of its performance.

**Rheology of Blood**

It has been mentioned previously that blood is a non-Newtonian fluid. Normal human blood possesses a distinctive yield stress. When the yield stress is exceeded, the same blood has a shear-stress shear-rate function closely following Casson's model, which implies reversible aggregation of red cells in rouleaux and flow dominated by movement of rouleaux [16]. Casson's equation [17] was first developed for pigment-oil suspensions and relates the rheological properties of a suspension composed of particles which are capable of aggregating into rodlike clusters.

\[
\tau_{yx} = \tau_0 + k \left( \frac{d\gamma}{dx} \right)^{\frac{1}{2}}
\]

Because of the formation of rouleaux by red blood cells [18], good correlation has been found between the rheological data taken on human blood with the Casson equation [19,20,21,22]. For banked-type O blood (containing ethylene-diamine tetraacetic acid as anticoagulant) the following empirical relations have been proposed [23]:

\[
\tau_0^{\frac{1}{2}} = (H - 0.017)^{1.55} \left( 1.55 C_f + 0.76 \right)
\]

\[
k = \left( \frac{\mu_0}{(1 - H)^{2.3}} \right)^{\frac{1}{2}}
\]
where \( \tau_0 \) = yield stress, dyne/cm\(^2\)

\( H \) = hematocrit (volume percent of red cells in whole blood)

\( C_F \) = fibrinogen concentration, g/100 ml

\( \mu_0 \) = viscosity of the suspending plasma, centipoise

\( j \) = a dimensionless constant of the order of unity, varying with the concentrations of the other plasma proteins.

For normal human blood at a hematocrit of 40, the average value of \( \tau_0 \) is 0.04 dyne/cm\(^2\) and the average value of \( k \) is 0.18 (g/sec-cm)\(^{1/2}\) [22,24].

**Two-Dimensional Blood Flow**

It has been pointed out that blood ultrafiltration involves two-dimensional flow of a non-Newtonian fluid. Because of the complexities involved, most analytical studies of blood flow have been greatly simplified. Blood flow in dialysis artificial kidneys has been treated as one-dimensional Newtonian flow in many papers [25,26,27]. Merrill [24], Aroesty [28], Kosijman [29], Shay [30] and Oka [34] used Casson's model in their blood flow analysis but their studies were limited to one-dimensional flow. Although there are many papers on the ultrafiltration of Newtonian flow between parallel plates and cylindrical pipes [31,32,33] no article on the ultrafiltration of non-Newtonian flow could be found in the literature.

The scope of this work will be confined to the simplest case of two-dimensional Cassonian flow, namely the ultrafiltration of blood between two parallel membranes with constant wall suction.
CHAPTER II

MATHEMATICAL DESCRIPTION OF THE PROBLEM

Statement of the Problem

The system under consideration, Figure 1, consists of a Cassonian fluid flowing downward between two parallel walls. At a certain point in the channel the walls become permeable. The flow is laminar and fully developed before the fluid contacts the walls that are permeable, and the dimensions of the channel are such that it can be considered semi-infinite.

Additional assumptions are:

(1) The fluid is Cassonian with constant physical properties.
(2) The flow is steady, isothermal and two-dimensional with velocity components in the x- and y-directions only.
(3) The wall suction rate is uniform and constant at each wall.
(4) There is no wall slip.
(5) The flow is symmetrical about the middle plane between the walls.

The purpose of this study is to establish for such a system velocity and pressure profiles at various mass flowrates, wall suction rates and yield stresses.
Figure 1. Schematic Drawing of the System.
Development of Casson's Model for Two-Dimensional Flow

For multidimensional, incompressible flow, Newton's law of viscosity is

\[ \tau = -\eta \Delta \]  \hspace{1cm} (2-1)

where \( \Delta \) is the symmetrical rate of deformation tensor with cartesian components \( \Delta_{ij} = (\partial v_i/\partial x_j) + (\partial v_j/\partial x_i) \). The coefficient of viscosity \( \eta \) is independent of \( \tau \) or \( \Delta \) for a Newtonian fluid.

For a non-Newtonian fluid, the relation between \( \tau \) and \( \Delta \) is

\[ \tau = -\eta \Delta \]  \hspace{1cm} (2-2)

where the non-Newtonian viscosity \( \eta \) is a scalar function of \( \Delta \) or \( \tau \). Consequently \( \eta \) must depend only on the invariants of \( \Delta \). The three invariants of \( \Delta \) are

\[ I_1 = (\Delta : \delta) = \sum_i \Delta_{ii} \]  \hspace{1cm} (2-3)

\[ I_2 = (\Delta : \Delta) = \sum_i \sum_j \sum_k \epsilon_{ijk} \Delta_{ij} \Delta_{jk} \]  \hspace{1cm} (2-4)

\[ I_3 = \det \Delta = \sum_i \sum_j \sum_k \epsilon_{ijk} \delta_{ij} \Delta_{1i} \Delta_{2j} \Delta_{3k} \]  \hspace{1cm} (2-5)

From the equation of continuity it can be shown that \( I_1 \) is always zero for incompressible fluids.
\[ I_1 = \sum_i \Delta_{ij} \]
\[ = \sum_i \left( \frac{\partial v_i}{\partial x_i} + \frac{\partial v_i}{\partial x_j} \right) \]
\[ = \sum_i 2 \left( \frac{\partial v_i}{\partial x_i} \right) \]
\[ = 2 (\Delta \cdot v) \]

But \((\Delta \cdot v) = 0\) for incompressible fluids, therefore

\[ I_1 = 0 \]

For many simple flows, the third invariant \(I_3\) either vanishes identically or can be assumed not very important. Therefore it is customary to assume \([35,36,37]\) that \(\eta\) can be taken to be a function of the second invariant \(I_2\).

The Casson equation for one-dimensional flow has been introduced in Chapter 1;

\[ \tau_{yx}^{\frac{1}{2}} = \tau_0^{\frac{1}{2}} + k \left( - \frac{dv_y}{dx} \right)^{\frac{1}{2}} \]  
(2-6)

Squaring the above equation:

\[ \tau_{yx} = \tau_0 + 2\tau_0^{\frac{1}{2}} k \left( - \frac{dv_y}{dx} \right)^{\frac{1}{2}} + k^2 \left( - \frac{dv_y}{dx} \right) \]  
(2-7)

According to Hohenemser \([35]\), the above equation can be written in the following tensor form for multidimensional flow:
\[ \tau = -[\tau_0 + 2\tau_0^{\frac{1}{2}} k \sqrt{\frac{1}{2} (\Delta : \Delta) \, \frac{1}{2} } \]
\[ + k^2 | \sqrt{\frac{1}{2} (\Delta : \Delta) | \frac{\Delta}{\sqrt{\frac{1}{2} (\Delta : \Delta)}} } \] \quad (2-8) \]

For two dimensional flow in the x- and y-directions:

\[ \frac{1}{2} (\Delta : \Delta) = [\left( \frac{\partial v}{\partial x} \right)^2 + \left( \frac{\partial v}{\partial y} \right)^2 ] + \left( \frac{\partial v}{\partial x} + \frac{\partial v}{\partial y} \right)^2 \] \quad (2-9) \]

Since this quantity will always be positive, substituting (2-9) into (2-8) gives

\[ \tau = -[\tau_0 (2[(\frac{\partial v}{\partial x})^2 + (\frac{\partial v}{\partial y})^2 ] + \frac{\partial v}{\partial x} \frac{\partial v}{\partial y} ] \]
\[ + \left[ \frac{\partial v}{\partial x} + \frac{\partial v}{\partial y} \right]^{\frac{1}{2}} \]
\[ + 2\tau_0^{\frac{1}{2}} k(2[(\frac{\partial v}{\partial x})^2 + (\frac{\partial v}{\partial y})^2 ]
\[ + \left[ \frac{\partial v}{\partial x} + \frac{\partial v}{\partial y} \right]^{\frac{1}{2}} + k^2 ) \Delta \] \quad (2-10) \]

For two-dimensional flow, the following stress components exist:

\[ \tau_{xx} = -[\tau_0 (2[(\frac{\partial v}{\partial x})^2 + (\frac{\partial v}{\partial y})^2 ] + \frac{\partial v}{\partial x} \frac{\partial v}{\partial y} ] \]
\[ + \left[ \frac{\partial v}{\partial x} + \frac{\partial v}{\partial y} \right]^{\frac{1}{2}} \]
\[ + 2\tau_0^{\frac{1}{2}} k(2[(\frac{\partial v}{\partial x})^2 + (\frac{\partial v}{\partial y})^2 ]
\[ + \left[ \frac{\partial v}{\partial x} + \frac{\partial v}{\partial y} \right]^{\frac{1}{2}} + k^2 \] \quad (2-11) \]
Fluid Flow Equations and Boundary Conditions

The system to be studied is represented in Figure 1. A Cassonian fluid with density $\rho$, yield stress $\tau_0$ and Casson viscosity $k^2$ is flowing downward between two parallel walls which change from non-permeable to permeable at a certain point down the stream. The rectangular coordinate system is used with $x$ measured from the initial end of the permeable walls down along the direction of the flow, and $y$ measured from the medium plane between the two parallel walls out toward the wall on the right. The distance between the two walls is $2H$ and the width is $W$. The initial volumetric flowrate is $Q_0$ and the initial pressure is $p_0$.

The governing equations for a multidimensional Cassonian flow are

\[ \tau_{yy} = -(\tau_0 \left(2\left[\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y}\right] + \left[\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y}\right]\right) - \frac{1}{2} k^2 \]

\[ + 2\tau_0 \frac{k}{2}\left[\left(\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y}\right) + \frac{\partial v_x}{\partial x} + \frac{\partial v_x}{\partial y}\right] - \frac{1}{2} k^2 \]

\[ + k^2 \left(\frac{\partial v_x}{\partial y} + \frac{\partial v_y}{\partial x}\right) \]
Equation of Continuity

\[(v \cdot v) = 0 \quad (2-14)\]

Equation of Motion

\[\rho \frac{Dv}{Dt} = -\nabla p - [v \cdot \tau] + \rho g \quad (2-15)\]

\[\tau = -\left\{ \frac{\tau_0}{\sqrt{\frac{1}{2} \langle \Delta, \Delta \rangle}} + \frac{2\tau_0 \frac{1}{2}k}{\sqrt{\frac{1}{2} \langle \Delta, \Delta \rangle}} \right\} \Delta \quad (2-16)\]

For steady two-dimensional Cassonian flow in the system described, the governing equations reduce to

Equation of Continuity

\[\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} = 0 \quad (2-17)\]

Equations of Motion

\[\rho(v \frac{\partial v_x}{\partial x} + v \frac{\partial v_x}{\partial y}) = -\frac{\partial p}{\partial x} - (\frac{\partial \tau_{xx}}{\partial x} + \frac{\partial \tau_{yx}}{\partial y}) + \rho g_x \quad (2-18)\]

\[\rho(v \frac{\partial v_y}{\partial x} + v \frac{\partial v_x}{\partial y}) = -\frac{\partial p}{\partial y} - (\frac{\partial \tau_{yx}}{\partial x} + \frac{\partial \tau_{yy}}{\partial y}) + \rho g_y \quad (2-19)\]

where as derived in (2-11), (2-12) and (2-13)
\[ \tau_{xx} = -\left( \tau_0 \left( 2 \left( \frac{\partial \nu_x}{\partial x} \right)^2 + \frac{\partial \nu_y}{\partial y} \right) \right) + \frac{\partial^{2}\nu_x}{\partial x^2} + \frac{\partial^{2}\nu_y}{\partial x \partial y} + \frac{\partial^{2}\nu_y}{\partial y^2} + \frac{\partial^{2}\nu_x}{\partial y^2} - \frac{1}{2} \]

\[ + 2\tau_0 k \left( 2 \left( \frac{\partial \nu_x}{\partial x} \right)^2 + \frac{\partial \nu_y}{\partial y} \right) \frac{\partial \nu_x}{\partial x} + \frac{\partial \nu_y}{\partial y} \frac{\partial \nu_x}{\partial y} + \frac{\partial \nu_y}{\partial y} \frac{\partial \nu_x}{\partial y} + \frac{\partial \nu_y}{\partial y} \frac{\partial \nu_x}{\partial y} + \frac{\partial \nu_x}{\partial x} - \frac{1}{2} \]

\[ + k^2 \left( 2 \frac{\partial \nu_x}{\partial x} \right) \]

\[ \tau_{yy} = -\left( \tau_0 \left( 2 \left( \frac{\partial \nu_x}{\partial x} \right)^2 + \frac{\partial \nu_y}{\partial y} \right) \right) + \frac{\partial^{2}\nu_y}{\partial x^2} + \frac{\partial^{2}\nu_y}{\partial x \partial y} + \frac{\partial^{2}\nu_y}{\partial y^2} + \frac{\partial^{2}\nu_x}{\partial y^2} - \frac{1}{2} \]

\[ + 2\tau_0 k \left( 2 \left( \frac{\partial \nu_x}{\partial x} \right)^2 + \frac{\partial \nu_y}{\partial y} \right) \frac{\partial \nu_y}{\partial x} + \frac{\partial \nu_x}{\partial x} \frac{\partial \nu_y}{\partial y} + \frac{\partial \nu_x}{\partial x} \frac{\partial \nu_y}{\partial y} + \frac{\partial \nu_x}{\partial x} \frac{\partial \nu_y}{\partial y} + \frac{\partial \nu_x}{\partial x} - \frac{1}{2} \]

\[ + k^2 \left( 2 \frac{\partial \nu_y}{\partial y} \right) \]

\[ \tau_{yx} = \tau_{xy} = -\left( \tau_0 \left( 2 \left( \frac{\partial \nu_x}{\partial x} \right)^2 + \frac{\partial \nu_y}{\partial y} \right) \right) + \frac{\partial^{2}\nu_y}{\partial x^2} + \frac{\partial^{2}\nu_y}{\partial x \partial y} + \frac{\partial^{2}\nu_y}{\partial y^2} + \frac{\partial^{2}\nu_x}{\partial y^2} - \frac{1}{2} \]

\[ + 2\tau_0 k \left( 2 \left( \frac{\partial \nu_x}{\partial x} \right)^2 + \frac{\partial \nu_y}{\partial y} \right) \frac{\partial \nu_y}{\partial x} + \frac{\partial \nu_x}{\partial x} \frac{\partial \nu_y}{\partial y} + \frac{\partial \nu_x}{\partial x} \frac{\partial \nu_y}{\partial y} + \frac{\partial \nu_x}{\partial x} \frac{\partial \nu_y}{\partial y} + \frac{\partial \nu_x}{\partial x} - \frac{1}{2} \]

\[ + k^2 \left( \frac{\partial \nu_x}{\partial x} + \frac{\partial \nu_y}{\partial y} \right) \]

**Boundary Conditions**

at \( y = 0 \), \( y = 0 \)

\[ \frac{\partial \nu_x}{\partial y} = 0 \]

and \( \tau_{yx} = \tau_{xy} = 0 \)

at \( y = \pm H \), \( \nu_y = \pm \nu_0 \) (constant)
\[ v_x = 0 \]

and \[ \tau_{xx} = 0 \]

at \( x = 0 \), \[ p = p_0 \]

and \[ 2W \int_0^H v_x dy = Q_0 \]

at \( x = x \), \[ 2W \int_0^H v_x dy = Q_0 - 2W \int_0^x v_y dx \]

Dimensionless Fluid Flow Equation and Boundary Conditions

To rewrite the flow equations and boundary conditions in dimensionless quantities, the average initial velocity \( U_0 = Q_0 / 2WH \) and the half distance \( H \) between the two parallel walls were chosen as reference quantities. The dimensionless variables are defined as follows

\[ T_0 = \frac{\tau_0}{\rho U_0^2} \quad K = \frac{k}{(\rho U_0 H)^{3/2}} \quad V_0 = \frac{v_0}{U_0} \]

\[ X = \frac{x}{H} \quad Y = \frac{y}{H} \]

\[ T_{xx} = \frac{\tau_{xx}}{\rho U_0^2} \quad T_{yy} = \frac{\tau_{yy}}{\rho U_0^2} \]

\[ T_{xy} = \frac{\tau_{xy}}{\rho U_0^2} \quad T_{yx} = \frac{\tau_{yx}}{\rho U_0^2} \]

\[ P = \frac{[p - \rho (g_x x + g_y y)]/\rho U_0^2}{ \rho U_0^2} \]

Substituting the above dimensionless variables into the previous equations and boundary conditions gives the following dimensionless flow equations and boundary conditions:
Equation of Continuity

$$\frac{\partial V_x}{\partial x} + \frac{\partial V_y}{\partial y} = 0 \quad (2-20)$$

Equation of Motion

$$V_x \frac{\partial V_x}{\partial x} + V_y \frac{\partial V_x}{\partial y} = -\frac{\partial P}{\partial x} - \left( \frac{\partial T_{xx}}{\partial x} + \frac{\partial T_{xy}}{\partial y} \right) \quad (2-21)$$

$$V_x \frac{\partial V_y}{\partial x} + V_y \frac{\partial V_y}{\partial y} = -\frac{\partial P}{\partial y} - \left( \frac{\partial T_{xy}}{\partial x} + \frac{\partial T_{yy}}{\partial y} \right) \quad (2-22)$$

where

$$T_{xx} = -(T_0 \left( 2 \left[ \frac{\partial V_x}{\partial x} \right]^2 + \left( \frac{\partial V_y}{\partial y} \right)^2 \right) + \left[ \frac{\partial V_x}{\partial y} + \frac{\partial V_y}{\partial x} \right]^2 - \frac{1}{2}$$

$$+ 2T_0 \left( \frac{\partial V_x}{\partial x}^2 + \left( \frac{\partial V_y}{\partial y} \right)^2 \right) + \left[ \frac{\partial V_x}{\partial y} + \frac{\partial V_y}{\partial x} \right]^2 \right)$$

$$+ K^2 \left( 2 \frac{\partial V_x}{\partial x} \right)$$

$$T_{yy} = -(T_0 \left( 2 \left[ \frac{\partial V_y}{\partial y} \right]^2 + \left( \frac{\partial V_x}{\partial x} \right)^2 \right) + \left[ \frac{\partial V_y}{\partial x} + \frac{\partial V_x}{\partial y} \right]^2 - \frac{1}{2}$$

$$+ 2T_0 \left( \frac{\partial V_y}{\partial y}^2 + \left( \frac{\partial V_x}{\partial x} \right)^2 \right) + \left[ \frac{\partial V_y}{\partial x} + \frac{\partial V_x}{\partial y} \right]^2 \right)$$

$$+ K^2 \left( 2 \frac{\partial V_y}{\partial y} \right)$$
\[ T_{yx} = T_{xy} = -T_0 \left( \frac{\partial V_y}{\partial x} \right)^2 - \left( \frac{\partial V_y}{\partial y} \right)^2 + \left( \frac{\partial V_x}{\partial x} + \frac{\partial V_y}{\partial y} \right)^2 - \frac{1}{\lambda} \]

\[ + 2T_0^{\frac{1}{2}} K \left( \frac{\partial V_x}{\partial x} \right)^2 + \left( \frac{\partial V_x}{\partial y} \right)^2 + \left( \frac{\partial V_y}{\partial x} \right)^2 - \frac{1}{\lambda} K^2 \left( \frac{\partial V_x}{\partial y} + \frac{\partial V_y}{\partial x} \right) \]

Boundary Conditions

at \( Y = 0 \),
\[ V_y = 0 \]
\[ \frac{\partial V_x}{\partial Y} = 0 \]
and
\[ T_{yx} = T_{xy} = 0 \]

at \( Y = \pm 1 \),
\[ V_y = \pm V_0 \]
\[ V_x = 0 \]
and
\[ T_{xx} = 0 \]

at \( X = 0 \),
\[ P = P_0 \]
and
\[ \int_0^1 V_x \, dY = 1 \]

at \( X = X \),
\[ \int_0^1 V_x \, dY = 1 - \int_0^X V_x \, dx \]
Equations in Terms of a Modified Dimensionless Stream Function and Stresses

Differentiating (2-21) with respect to $Y$, differentiating (2-22) with respect to $X$ and combining the two resulting equations to eliminate the pressure terms gives

$$\frac{\partial}{\partial Y} \left( v_x \frac{\partial v_x}{\partial X} + v_y \frac{\partial v_x}{\partial Y} \right) - \frac{\partial}{\partial X} \left( v_x \frac{\partial v_y}{\partial X} + v_y \frac{\partial v_y}{\partial Y} \right)$$

$$= \frac{\partial}{\partial X} \left( \frac{\partial T_{XY}}{\partial Y} + \frac{\partial T_{XY}}{\partial Y} \right) - \frac{\partial}{\partial Y} \left( \frac{\partial T_{XX}}{\partial X} + \frac{\partial T_{YY}}{\partial Y} \right)$$

(2-26)

Now assume a modified dimensionless stream function $\psi$ which is defined by the following relations:

$$v_x = \frac{\partial \psi}{\partial Y} \quad v_y = -\frac{\partial \psi}{\partial X}$$

With the above definition, $v_x$ and $v_y$ automatically satisfy the equation of continuity (2-20).

Introducing the stream function $\psi$ into (2-26) gives

$$\left( \frac{\partial \psi}{\partial Y} \right) \left[ \frac{\partial}{\partial X} \left( \frac{\partial \psi}{\partial Y} \right) + \frac{\partial^2 \psi}{\partial X^2} \right] - \left( \frac{\partial \psi}{\partial X} \right) \left[ \frac{\partial}{\partial Y} \left( \frac{\partial \psi}{\partial Y} \right) + \frac{\partial^2 \psi}{\partial Y^2} \right]$$

$$= \frac{\partial}{\partial X} \left( \frac{\partial T_{XY}}{\partial Y} + \frac{\partial T_{XY}}{\partial Y} \right) - \frac{\partial}{\partial Y} \left( \frac{\partial T_{XX}}{\partial X} + \frac{\partial T_{YY}}{\partial Y} \right)$$

(2-27)

The left side of (2-26) can be written in a more conventional form

$$\frac{\partial (\psi, \psi^2)}{\partial (X,Y)} = \frac{\partial}{\partial X} \left( \frac{\partial T_{XY}}{\partial Y} + \frac{\partial T_{XY}}{\partial Y} \right) - \frac{\partial}{\partial Y} \left( \frac{\partial T_{XX}}{\partial X} + \frac{\partial T_{YY}}{\partial Y} \right)$$

(2-28)

where
\[
\frac{\partial (\psi, \nabla^2 \psi)}{\partial (X, Y)} = \begin{pmatrix} \frac{\partial \psi}{\partial X} \\ \frac{\partial \psi}{\partial Y} \\ \frac{\partial (\nabla^2 \psi)}{\partial X} \\ \frac{\partial (\nabla^2 \psi)}{\partial Y} \end{pmatrix}
\]

and

\[
\nabla^2 \psi = \frac{\partial^2 \psi}{\partial X^2} + \frac{\partial^2 \psi}{\partial Y^2}
\]

Introducing the stream function $\psi$ into (2-23), (2-24) and (2-25) gives

\[
T_{xx} = -\left( T_0 \left[ 4 \left( \frac{\partial^2 \psi}{\partial X \partial Y} \right)^2 + \left( \frac{\partial^2 \psi}{\partial Y^2} - \frac{\partial^2 \psi}{\partial X^2} \right)^2 \right] \right)^{-\frac{1}{2}} + 2T_0 K \left[ 4 \left( \frac{\partial^2 \psi}{\partial X \partial Y} \right)^2 + \left( \frac{\partial^2 \psi}{\partial Y^2} - \frac{\partial^2 \psi}{\partial X^2} \right)^2 \right]^{-\frac{1}{2}}
\]

\[
+ K^2 \left\{ 2 \frac{\partial^2 \psi}{\partial X \partial Y} \right\}
\]

\[
T_{yy} = -\left( T_0 \left[ 4 \left( \frac{\partial^2 \psi}{\partial X \partial Y} \right)^2 + \left( \frac{\partial^2 \psi}{\partial Y^2} - \frac{\partial^2 \psi}{\partial X^2} \right)^2 \right] \right)^{-\frac{1}{2}} + 2T_0 K \left[ 4 \left( \frac{\partial^2 \psi}{\partial X \partial Y} \right)^2 + \left( \frac{\partial^2 \psi}{\partial Y^2} - \frac{\partial^2 \psi}{\partial X^2} \right)^2 \right]^{-\frac{1}{2}}
\]

\[
+ K^2 \left\{ -2 \frac{\partial^2 \psi}{\partial X \partial Y} \right\}
\]

\[
T_{yx} = T_{xy} = -\left( T_0 \left[ 4 \left( \frac{\partial^2 \psi}{\partial X \partial Y} \right)^2 + \left( \frac{\partial^2 \psi}{\partial Y^2} - \frac{\partial^2 \psi}{\partial X^2} \right)^2 \right] \right)^{-\frac{1}{2}} + 2T_0 K \left[ 4 \left( \frac{\partial^2 \psi}{\partial X \partial Y} \right)^2 + \left( \frac{\partial^2 \psi}{\partial Y^2} - \frac{\partial^2 \psi}{\partial X^2} \right)^2 \right]^{-\frac{1}{2}}
\]

\[
+ K^2 \left\{ \frac{\partial^2 \psi}{\partial Y^2} - \frac{\partial^2 \psi}{\partial X^2} \right\}
\]
By (2-29) and (2-30)

\[ T_{xx} = -T_{yy} \quad (2-32) \]

This relation can also be proved with stress equations (2-23), (2-24), and the equation of continuity (2-20) in terms of velocity components. Substituting (2-32) into (2-28) gives

\[ 2^* \frac{\partial^2 T_{yx}}{\partial y^2} = 2 \frac{\partial^2 T_{yx}}{\partial x^2} + 2 \frac{\partial^2 T_{xx}}{\partial x \partial y} \quad (2-33) \]

The assumption of creeping flow greatly simplifies the above equation without seriously restricting the utility of the results [38]. By assuming creeping flow, the left side of (2-33) may be neglected. After rearranging

\[ \frac{\partial^2 T_{yx}}{\partial y^2} - \frac{\partial^2 T_{yx}}{\partial x^2} + 2 \frac{\partial^2 T_{xx}}{\partial x \partial y} = 0 \quad (2-34) \]

Dividing (2-29) by (2-30) gives

\[ \frac{T_{xx}}{T_{yx}} = \frac{2 \frac{\partial^2 \psi}{\partial x \partial y}}{2 \frac{\partial^2 \psi}{\partial y^2} - \frac{\partial^2 \psi}{\partial x^2}} \]

\[ = \frac{2F^2 \psi}{D^2 \psi} = 2 \gamma \]

where
Substituting (2-35) into (2-34) gives

$$2F^2 \left( \frac{\partial^2 T}{\partial \psi \partial Ix} \right) + D^2 \frac{\partial^2 T}{\partial \psi \partial Ix} = 0 \quad (2-36)$$

where

$$T_{yx} = \{ T_0 [4(F^2 \psi)^2 + (D^2 \psi)^2]^{-\frac{1}{2}} + 2T_0 \frac{1}{\sqrt{2}} K[4(F^2 \psi)^2 + (D^2 \psi)^2]^{-\frac{1}{2}} + K^2 \} (D^2 \psi) \quad (2-37)$$

Equations (2-36) and (2-37) are to be solved with the following boundary conditions:

at \( Y = 0 \),\[
\begin{align*}
\psi &= 0 , \\
\frac{\partial^2 \psi}{\partial Y^2} &= 0 \\
T_{yx} &= 0
\end{align*}
\]

and

at \( Y = 1 \),\[
\begin{align*}
\psi &= 1 - V_0 X , \\
\frac{\partial \psi}{\partial Y} &= 0 \\
T_{yx} &= F(\psi) |_{Y=1}
\end{align*}
\]
at $X = 0$, 

$$
\psi = \frac{Y}{K^2} \left( \frac{1}{2} T_0 (1 - \frac{Y^2}{3}) - \frac{4}{3} T_0 \frac{1}{2} P_f^{\frac{1}{2}} (1 - \frac{2}{5} Y^{3/2}) \right) + T_0 (1 - \frac{1}{2}) 
$$

and 

$$
T_{y\chi} = P_f Y 
$$

where 

$$
P_f^{\frac{1}{2}} = \frac{6}{5} T_0^{\frac{1}{2}} + (3K^2 - \frac{3}{50} T_0)^{\frac{1}{2}} 
$$

*Derivations of equations (2-38), (2-39) and (2-40) are presented in Appendix A.*
CHAPTER III

NUMERICAL TECHNIQUE

It is often very difficult or even impossible to obtain analytical solutions for fluid flow problems that involve complicated partial differential equations such as those developed in this study. However, the numerical approximation method coupled with the high-speed electronic computer can in many cases give numerical solutions at predetermined points in the domain of interest which are sufficient for engineering design and analysis. The numerical techniques used in this study are "finite difference approximations," "the relaxation method," "Newton-Raphson iteration" and "the method of false position" [39,40,41,42].

Mathematical Derivation of Finite Difference
Differentiation and Graphical Interpretations

Finite difference approximation converts differential equations into algebraic equations which correlate the functional values of the neighboring points. In doing this, each differential term in the differential equation is replaced with a corresponding finite difference approximation. Such finite difference approximations can be obtained from Taylor's series.

Referring to Figure 2, \( y = f(x) \) is a function represented by the curve ABC whose first derivative we wish to approximate. Dividing the \( x \) coordinate into equal increments of \( \Delta x \)
\[ x_I = I \Delta x , \]
\[ f_I = f(x_I) = f(I \Delta x) \quad \text{and} \]
\[ f_{I+1} = f(x_{I+1}) = f(I \Delta x + \Delta x) \]

From Taylor's series expansion

\[ f_{I-1} = f_I - \Delta x \frac{df}{dx} \bigg|_I + \frac{\Delta x^2}{2!} \frac{d^2f}{dx^2} \bigg|_I - \frac{\Delta x^3}{3!} \frac{d^3f}{dx^3} \bigg|_I + \frac{\Delta x^4}{4!} \frac{d^4f}{dx^4} \bigg|_I - \ldots \quad (3-1) \]

\[ f_{I+1} = f_I + \Delta x \frac{df}{dx} \bigg|_I + \frac{\Delta x^2}{2!} \frac{d^2f}{dx^2} \bigg|_I + \frac{\Delta x^3}{3!} \frac{d^3f}{dx^3} \bigg|_I + \frac{\Delta x^4}{4!} \frac{d^4f}{dx^4} \bigg|_I + \ldots \quad (3-2) \]

As long as \( \Delta x \) is sufficiently small, terms of the order of \( \Delta x^2 \) and higher may be neglected. Then from equation (3-1), we get the following approximation

\[ \frac{df}{dx} \bigg|_I = \frac{f_I - f_{I-1}}{\Delta x} + O(\Delta x) \quad (3-3) \]

or from equation (3-2)

\[ \frac{df}{dx} \bigg|_I = \frac{f_{I+1} - f_I}{\Delta x} + O(\Delta x) \quad (3-4) \]

If equation (3-2) is subtracted from equation (3-1) and neglecting the \( \Delta x^3 \) and higher order terms, we get a better approximation because we do not have to neglect the \( \Delta x^2 \) terms.
Figure 2. Graphical Interpretation of Finite Difference Differentiation.
\[
\frac{df}{dx}\bigg|_I = \frac{f_{I+1} - f_{I-1}}{2\Delta x} + O(\Delta x) \quad (3-5)
\]

where \(O(\Delta x^n)\) is the truncation error involved in neglecting the terms of the order of \(\Delta x^{n+1}\) and higher. \(O(\Delta x^n)\) can usually be neglected when \(\Delta x\) is sufficiently small.

The approximations in equations (3-3), (3-4) and (3-5) can also be obtained graphically (Figure 2). By definition, \(df/dx\big|_I\) is the slope of the tangent line LM. This slope can be approximated by the slope of line AB or line BC and best by the slope of line AC. When \(\Delta x\) becomes smaller, these slopes approach the true slope of the tangent line LM. These slopes are

for AB \(\frac{df}{dx}\big|_I = \frac{f_{I} - f_{I-1}}{\Delta x} \quad (3-3A)\)

for BC \(\frac{df}{dx}\big|_I = \frac{f_{I+1} - f_{I}}{\Delta x} \quad (3-4A)\)

for AC \(\frac{df}{dx}\big|_I = \frac{f_{I+1} - f_{I-1}}{2\Delta x} \quad (3-5A)\)

Equations (3-3A), (3-4A) and (3-5A) are equivalent to equations (3-3), (3-4) and (3-5) with the truncation terms \(O(\Delta x^n)\) neglected.

Adding equations (3-1) and (3-2) and neglecting \(\Delta x^3\) and higher order terms we get

\[
\frac{d^2f}{dx^2}\bigg|_I = \frac{f_{I+1} - 2f_{I} + f_{I-1}}{\Delta x^2} + O(\Delta x^2) \quad (3-6)
\]
Graphically this approximation can also be derived from the slopes.

\[
\frac{d^2f}{dx^2}\bigg|_I = \frac{df}{dx}\bigg|_I = \frac{f_{I+1/2} - f_{I-1/2}}{\Delta x}
\]  

(3-7)

where \(f_{I+1/2}\) and \(f_{I-1/2}\) are the slopes of the curve at \(x_{I+1/2}\) and \(x_{I-1/2}\) which can be approximated by the slopes of BC and AB.

\[
f_{I+1/2} = \frac{df}{dx}\bigg|_{I+1/2} = \frac{f_{I+1} - f_I}{\Delta x}
\]  

(3-8)

\[
f_{I-1/2} = \frac{df}{dx}\bigg|_{I-1/2} = \frac{f_I - f_{I-1}}{\Delta x}
\]  

(3-9)

Substituting equations (3-8) and (3-9) into equation (3-7) we get

\[
\frac{d^2f}{dx^2}\bigg|_I = \frac{f_{I+1} - 2f_I + f_{I-1}}{\Delta x^2}
\]  

(3-6A)

Again (3-6A) is equivalent to (3-6) with the truncation term \(O(\Delta x^2)\) neglected.

The derivation procedure used in equations (3-7), (3-8), (3-9) and (3-6A) will be used in deriving approximations to partial derivatives with respect to two independent variables in the next section.

**System of Grid Points and Two-Dimensional Partial Derivatives**

Consider a function \(f(X,Y)\) which depends on both \(X\) and \(Y\). Cover the \(X-Y\) plane with a rectangular grid system as shown in Figure 3 so
Figure 3. System of Grid Points.
that the grid point \((I,J)\) is equivalent to the space point \((I\Delta X, J\Delta Y)\) and the value of the variable \(f(X,Y)\) on this grid point is \(f_{I,J} = f(I\Delta X, J\Delta Y)\). The neighboring grid points are labeled \((I+1,J), (I-1,J), (I,J+1), (I,J-1), (I+1,J+1), (I+1,J-1), (I-1,J-1)\) and \((I-1,J+1)\) as shown in Figure 3.

Letting \(\Delta X = k, \Delta Y = h\) and \(k = sh\), the partial derivatives can be approximated according to (3-5A) and (3-6A) as

\[
\frac{\partial f}{\partial x}_{I,J} = \frac{f_{I+1,J} - f_{I-1,J}}{2k} = \frac{f_{I+1,J} - f_{I-1,J}}{2sh} \quad (3-7)
\]

\[
\frac{\partial f}{\partial y}_{I,J} = \frac{f_{I,J+1} - f_{I,J-1}}{2h} \quad (3-8)
\]

\[
\frac{\partial^2 f}{\partial x^2}_{I,J} = \frac{f_{I+1,J} - 2f_{I,J} + f_{I-1,J}}{k^2} = \frac{f_{I+1,J} - 2f_{I,J} + f_{I-1,J}}{s^2h^2} \quad (3-9)
\]

\[
\frac{\partial^2 f}{\partial y^2}_{I,J} = \frac{f_{I,J+1} - 2f_{I,J} + f_{I,J-1}}{h^2} \quad (3-10)
\]

The derivative \(\partial^2 f/\partial x \partial y\) can be approximated by a procedure similar to the steps taken in deriving (3-6A)
\[
\frac{\partial^2 f}{\partial x \partial y} \bigg|_{I,J} = \frac{\partial}{\partial x} \left( \frac{\partial f}{\partial y} \right) \bigg|_{I,J}
\]
\[
= \frac{\partial f}{\partial y} \bigg|_{I+1,J} - \frac{\partial f}{\partial y} \bigg|_{I-1,J}
\]
\[
= \frac{1}{2h} \left( \frac{f_{I+1,J+1} - f_{I+1,J-1}}{2h} - \frac{f_{I-1,J+1} - f_{I-1,J-1}}{2h} \right)
\]
\[
\frac{\partial^2 f}{\partial x \partial y} \bigg|_{I,J} = \frac{1}{4sh^2} \left( f_{I+1,J+1} + f_{I-1,J+1} - f_{I+1,J-1} - f_{I-1,J-1} \right) \tag{3-11}
\]

**Finite Difference Flow Equations**

From equations (3-7), (3-8), (3-9), (3-10) and (3-11) we can write

\[
F^2(\gamma T) \bigg|_{I,J} = \frac{\partial^2}{\partial x \partial y} \left( \gamma T \right) \bigg|_{I,J} \tag{3-12}
\]
\[
= \frac{1}{4sh^2} \left[ (\gamma T)_{I+1,J+1} + (\gamma T)_{I-1,J-1} - (\gamma T)_{I+1,J-1} - (\gamma T)_{I-1,J+1} \right]
\]

where \( T = T_{yx} \)

\[
D^2 T \bigg|_{I,J} = \left( \frac{\partial^2}{\partial y^2} - \frac{\partial^2}{\partial x^2} \right) T \bigg|_{I,J} \tag{3-13}
\]
\[
= \frac{1}{s^2 h^2} \left[ s^2 (T_{I,J+1} + T_{I,J-1}) - 2(s^2 - 1)T_{I,J} - T_{I+1,J} - T_{I-1,J} \right]
\]

Substituting (3-12) and (3-13) into (2-36)
\[s[(\gamma I)_{I+1,J+1} + (\gamma I)_{I-1,J-1} - (\gamma I)_{I+1,J-1} + (\gamma I)_{I-1,J+1} + s^2(T_{I,J+1} + T_{I,J-1}) - 2(s^2 - 1)T_{I,J} - T_{I+1,J} - T_{I-1,J} = 0 \]  

Equation (3-14) can be rewritten in the following form

\[s[(\gamma I+1,J+1)(T_{I+1,J+1}) + (\gamma I-1,J-1)(T_{I-1,J-1}) - (\gamma I+1,J-1)(T_{I+1,J-1}) - (\gamma I-1,J+1)(T_{I-1,J+1}) + s^2(T_{I,J+1} + T_{I,J-1}) - 2(s^2 - 1)T_{I,J} - T_{I+1,J} - T_{I-1,J} = 0 \]  

where

\[\gamma I,J = \frac{F^2 \psi}{\partial^2 \psi}|_{I,J} = \frac{(F^2 \psi)_{I,J}}{(D^2 \psi)_{I,J}} \]

and

\[(F^2 \psi)_{I,J} = \frac{1}{4sh^2} (\psi_{I+1,J+1} + \psi_{I-1,J-1} - \psi_{I+1,J-1} - \psi_{I-1,J+1})\]

\[(D^2 \psi)_{I,J} = \frac{1}{s^2 h^2} [s^2(\psi_{I,J+1} + \psi_{I,J-1}) - 2(s^2 - 1)\psi_{I,J} - \psi_{I+1,J} - \psi_{I-1,J}]\]
Rearranging equation (3-15), we get

\[ T_{I+1,J} = s^2(T_{I,J+1} + T_{I,J-1}) - 2(s^2 - 1)T_{I,J} \quad (3-16) \]

or

\[ T_{I+1,J} = T_{I+1,J} + \alpha(s^2(T_{I,J+1} + T_{I,J-1})) \]

\[ - 2(s^2 - 1)T_{I,J} - T_{I+1,J} - T_{I-1,J} \]

\[ - s[(\gamma_{I+1,J+1})(T_{I+1,J+1})] \]

\[ + (\gamma_{I-1,J-1})(T_{I-1,J-1}) - (\gamma_{I+1,J-1})(T_{I+1,J-1}) \]

\[ - (\gamma_{I-1,J+1})(T_{I-1,J+1})] \]

where \( \alpha \) is a relaxation factor, found by trial, for faster convergence.

Now rewrite equation (2-37) in the finite difference form

\[ T_{I,J} = - \{(T_0[4(F^2 \phi)_{I,J}^2 + (D^2 \phi)_{I,J}^2]^{-2} \]

\[ + 2T_0^{-1}K[4(F^2 \psi)_{I,J}^2 + (D^2 \psi)_{I,J}^2]^{-1} \]

\[ + K^2 \} (D^2 \psi)_{I,J} \]

\[ (3-18) \]
where again

\[
(F^2\psi)_{I,J} = \frac{1}{4\sin^2} (\psi_{I+1,J+1} + \psi_{I-1,J-1} - \psi_{I+1,J-1} - \psi_{I-1,J+1})
\]

\[
(D^2\psi)_{I,J} = \frac{1}{2 \sin^2} [s^2(\psi_{I,J+1} + \psi_{I,J-1}) - 2(s^2 - 1)\psi_{I,J} - \psi_{I+1,J} - \psi_{I-1,J}]
\]

Equation (3-18) cannot be expressed explicitly for \(\psi_{I+1,J}\). Iterative methods have to be used.

**Newton-Raphson Iteration**

Let

\[
F(\psi_{I+1,J}) = \left( T_0 [4(F^2\psi)_{I,J}^2 + (D^2\psi)_{I,J}^2]^{1/2} \right.
\]

\[
+ 2 T_0^{1/2} K[4(F^2\psi)_{I,J}^2 + (D^2\psi)_{I,J}^2]^{-1/2}
\]

\[
+ K^2 \right) (D^2\psi)_{I,J} + \psi_{I,J}
\]

then

\[
F'(\psi_{I+1,J}) = \frac{\partial F(\psi_{I+1,J})}{\partial \psi_{I+1,J}}
\]

\[
= (T_0 [4(F^2\psi)_{I,J}^2 + (D^2\psi)_{I,J}^2]^{-1/2}
\]

\[
+ 2 T_0^{1/2} K[4(F^2\psi)_{I,J}^2 + (D^2\psi)_{I,J}^2]^{-3/2}
\]

\[
+ (T_0 [4(F^2\psi)_{I,J}^2 + (D^2\psi)_{I,J}^2]^{-3/2}
\]

\[
+ T_0^{1/2} K[4(F^2\psi)_{I,J}^2 + (D^2\psi)_{I,J}^2]^{-5/4} \left[ \frac{(D^2\psi)_{I,J}^2}{\sin^2} \right]
\]
The value of $F(\psi^{I+1,J})$ approaches zero when $\psi^{I+1,J}$ approaches a value that satisfies equation (3-18). To find this value of $\psi^{I+1,J}$, a first estimation $\psi^{0}_{I+1,J}$ is made, then the next improved estimation is

$$
\psi^{1}_{I+1,J} = \psi^{0}_{I+1,J} - \frac{F(\psi^{0}_{I+1,J})}{F'(\psi^{0}_{I+1,J})} \quad (3-21)
$$

Repeating this process

$$
\psi^{m+1}_{I+1,J} = \psi^{m}_{I+1,J} - \frac{F(\psi^{m}_{I+1,J})}{F'(\psi^{m}_{I+1,J})} \quad (3-22)
$$

for $m = 0, 1, 2, 3 \ldots$

until

$$
|\psi^{m}_{I+1,J} - \psi^{m}_{I+1,J}| < \varepsilon
$$

Where $\varepsilon$ is a arbitrarily chosen small value. This process is illustrated in Figure 4. While Newton-Raphson iteration usually converges quite fast, it is unstable in some cases as shown in Figure 5.

**The Method of False Position**

This method is illustrated in Figure 6. The algorithm is contained in the following sequence of steps:

**Step 1.** Choose two approximations $\psi^{0}_{I+1,J}$ and $\psi^{1}_{I+1,J}$ such that

$$(\psi^{0}_{I+1,J})(\psi^{1}_{I+1,J}) < 0$$

**Step 2.** Find a next approximation from the formula

$$
\psi^{2}_{I+1,J} = \frac{(\psi^{0}_{I+1,J})F(\psi^{1}_{I+1,J}) - (\psi^{1}_{I+1,J})F(\psi^{0}_{I+1,J})}{F(\psi^{1}_{I+1,J}) - F(\psi^{0}_{I+1,J})} \quad (3-23)
$$
Figure 4. Newton-Raphson Iteration.
Figure 5. Newton-Raphson Iteration Fails to Converge.
Figure 6. The Method of False Position.
Step 3. If $|\psi_{I+1,J}^2 - \psi_{I+1,J}^0| < \epsilon$ or if $|\psi_{I+1,J}^2 - \psi_{I+1,J}^0| < \epsilon$
for a prescribed $\epsilon$, $\psi_{I+1,J}^2$ is accepted as the answer.
If not, go to Step 4.

Step 4. If $F(\psi_{I+1,J}^2)F(\psi_{I+1,J}^0) < 0$, replace $\psi_{I+1,J}^0$ by $\psi_{I+1,J}^2$,
leave $\psi_{I+1,J}^0$ unchanged and compute the next approximation from equation (3-23). Otherwise replace
$\psi_{I+1,J}^0$ by $\psi_{I+1,J}^1$, leave $\psi_{I+1,J}^0$ unchanged and compute
the next approximation from (3-23).

Although this method usually does not converge as fast as the
Newton-Raphson method, it is more stable and always converges to the
solution value if the function changes sign around this value.

If a solution to equation (3-18) is found to be $\psi_{I+1,J}^*$, then it
will be used in the following equation to carry out the relaxation
process

$$\psi_{I+1,J}^1 = \psi_{I+1,J}^0 + \beta(\psi_{I+1,J}^* - \psi_{I+1,J}^0)$$

(3-24)

where $\beta$ is the relaxation factor. A successive relaxation method
[39,42] will be used to calculate the values of $T_{I+1,J}$ and $\psi_{I+1,J}$ from
equations (3-17) and (3-24).

**Computational Procedures**

Most of the calculations were carried out with a Univac-1108
electronic digital computer. The computer programs involved are pre-
sented in Appendix B. The following logic steps were taken in computing
the desired quantity:
(1) Calculate initial values of $\psi$ and $T$ with equations (2-38) and (2-39). These are the stream functions and shear stresses of a one-dimensional Cassonian flow between two parallel plates with nonpermeable walls. Mathematical operations in obtaining equations (2-38) and (2-39) are presented in Appendix A.

(2) The stream function $\psi$ and the shear stress $T$ on the central plane, which is the lower boundary of the flow field to be studied, are set equal to zero.

(3) The stream function on the upper permeable wall, which is the upper boundary of the flow field to be studied, is calculated according to the boundary condition $\psi = 1 - V_0 x$ on the permeable wall.

(4) In order to reduce the number of iterations needed, a first estimation of $\psi_{I,J}$ is made by the following relation

$$\psi_{I,J} = \left( \frac{\psi_{I, \text{wall}}}{\psi_{0, \text{wall}}} \right) \psi_{0,J}$$

(5) New values of $\psi$ on the first line are calculated with iteration equations (3-22) and (3-24) until the difference in the values of $\psi$ between two successive iterative steps is less than $\varepsilon_1$ (input data) at each interior point on the first line.

(6) New values of $\psi$ in the downstream flow field are calculated by iteration equations (3-23) and (3-24).

(7) New values of $T$ are calculated by equation (3-17).
CHAPTER IV

RESULTS AND DISCUSSION

The present chapter is devoted to the presentation and discussion of numerical experiments on the ultrafiltration of a Cassonian fluid between two parallel membranes. The greatest portion of the numerical calculations was carried out with the aid of a Univac-1108 electronic digital computer at the Georgia Institute of Technology Rich Electronic Computer Center. A small portion of the calculations was made on the CDC CYBER 74 electronic digital computer after the Computer Center made the change from Univac to CDC.

Various rectangular grid steps were used to test the accuracy of the calculations. It was found that 100 grid points in the X-direction and 25 grid points in the Y-direction were sufficiently small to give excellent results. The X to Y grid step ratio, s, used in the calculations was 25, which was close to the maximum value that would not affect the convergence of the iteration process.

The results were plotted with a Calcomp plotter and are presented graphically. Five different types of plots are presented for the easy visualization of the effect of the different variables on the flow. The five types of plots are: (1) streamlines and shear-stress contours in the XY plane, (2) stream function and shear stress in steps of X vs Y, (3) $V_x$ in steps of X vs Y, (4) pressure on the central plane vs X, (5) $V_y$ in steps of X vs Y.
The streamline and shear-stress contours were plotted with the aid of the GPCP (General Purpose Contouring Program) program by California Computer Products [43].

The half distances between the parallel membranes are 0.005 cm, 0.01 cm and 0.05 cm. The entrance Reynolds number \( R_x (4\nu_0 H_0/k^2) \) covers the range from 0.25 to 25. The wall Reynolds number \( R_y (\nu_0 H_0/k^2) \) covers the range from zero to 0.025 (Tables 1, 2).

Results are presented and discussed in four sections: (1) Comparison of iterative and analytical results in limiting cases. (2) Effect of wall suction rate on the flow. (3) Effect of finite yield stress on the flow. (4) Some mutually related variables.

Comparison of Iterative and Analytical Results in Limiting Cases

It is difficult to make a truly comparative evaluation of this study because no experimental or other numerical work could be found on two-dimensional Cassonian flow. However, the logic and validity of the computational procedures can be checked out in two ways.

(1) By setting the finite shear stress \( \tau_0 \) to zero in the input data, the problem is reduced to a two-dimensional Newtonian flow whose analytical solution can be obtained as the following equation:

\[
\psi = \frac{y}{2} (3 - y^3)(1 - \nu_0 x)
\]  
(3-25)

A comparison of the values calculated with the equation above and the values obtained with the iterative procedure at selected grid points is presented in Table 3. It can be seen that the agreement is excellent. Only the last two digits differ from the analytical values.
Table 1. Values of Variables Studied in Cassonian Flow

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Table 2. Values of Variables Studied in Newtonian Flow

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Table 3. Comparison of Iterative and Analytical Values of \( \psi \)
Case 1: Reduced to Newtonian Flow
\( (r_0 = 0; \ H = 0.01; \ R_x = 1.00; \ R_y = 0.001) \)

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<td>0.340800</td>
<td>0.475203</td>
<td>0.566400</td>
<td>0.600000</td>
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at but a few grid points in the worst cases.

(2) By setting the wall flux velocity \( v_0 \) equal to zero \( (R_y = 0) \) in the input data, the problem is reduced to a one-dimensional Cassonian flow whose analytical solution is derived in Appendix A as:

\[
\psi = \frac{\gamma}{K^2} \left[ \frac{1}{2} p_f (1 - \frac{\gamma}{3}) - \frac{4}{3} T_o^{1/2} P_f^{1/2} (1 - \frac{2}{5} \gamma^{3/2}) \right] + T_o (1 - \frac{\gamma}{2})
\]

\[ \text{(3-26)} \]

where

\[
p_f = \frac{6}{5} T_o^{1/2} + (3K^2 - \frac{3}{50} T_o^{1/2})
\]

\[ \text{(3-27)} \]

A comparison of the values calculated with the equation above and the values obtained with the iterative procedure at selected grid points is presented in Table 4. The analytical value is a function of \( \gamma \) only since there is no wall flux. The iterative value did change between \( X = 0 \) and \( X = 20 \) but stabilized with greater \( X \) values. The largest deviation of the iterative value from the analytical value is somewhat larger than in the Case 1 comparison but is still less than 0.05% from the analytical value. The agreement can still be considered excellent.

The excellent results of the two comparisons made above indicate that the logic and iterative procedures developed in this study are valid and sound.

**Effect of Finite Yield Stress (\( \tau_0 \))**

The finite yield stress \( \tau_0 \) is a characteristic term in the Casson equation (1-1). The average value of \( \tau_0 \) is 0.04 dyne/cm² for normal
Table 4. Comparison of Iterative and Analytical Values of $\psi$
Case 2: Reduced to One-Dimensional Flow

($r_o = 0.04; H = 0.01; R_x = 1.00; R_y = 0.00$)

<table>
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</tr>
<tr>
<td>I 40</td>
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<tr>
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human blood. To study the effect of this variable on the flow, four
other values of $\tau_0$ were assumed. They are 0, 0.01, 0.08 and 0.2. All
other variables were kept the same so that the effect of $\tau_0$ could be
isolated. The half distance between the two membranes was 0.01 cm.
The entrance Reynolds number ($R^\infty_x$) was 1.0 and the wall Reynolds number
was 0.001. The results are presented in the following groups of plots:

(1) The contours of stream function ($\psi$) and shear stress ($T_{yx}$)
in the XY plane are presented in Figures 7 through 11. In Figure 7, $\tau_0$
takes the value of zero and hence the yield stress term no longer exists.
This reduces the flow to a Newtonian flow and this plot is essentially
identical to the plot in Figure 7a which was made from the analytical
solution of a two-dimensional creeping Newtonian flow. As the value of
$\tau_0$ increases from zero to 0.2, the changes in stream line contours are
too small to be observed in these plots while the shear-stress contours
move in from the wall appreciably indicating an increase in shear stress
when the value of the finite stress term $\tau_0$ increases.

(2) The stream function ($\psi$) and shear stress ($T_{yx}$) at selected
values of $X$ are plotted against $Y$ in Figures 12 through 16. It can be
observed that both the stream function ($\psi$) and the shear stress ($T_{yx}$)
decrease with increasing values of $X$ down the stream. The plot in
Figure 12 is again reduced to that of a Newtonian flow with $\tau_0$ set equal
to zero. This plot is essentially the same as the plot in Figure 36
which was plotted from the analytical solution of a two-dimensional
Newtonian flow. It can be seen in Figures 12 through 16 that the shear
stress increases with increasing values of $\tau_0$. 
Figure 7. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Cassonian: $H = 0.01$  \hspace{1cm} $\tau_0 = 0$

$R_x = 1.0$  \hspace{1cm} $R_y = 0.001$
Figure 7a. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Newtonian: $H = 0.01 \quad R_x = 1.0 \quad R_y = 0.001$
Figure 8. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Cassonian: $H = 0.01$ \hspace{1cm} $\tau_0 = 0.01$

$R_x = 1.0$ \hspace{1cm} $R_y = 0.001$
Figure 9. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Cassonian: $H = 0.01$  $R_x = 1.0$  $R_y = 0.01$

$\phi = 0.20$  $T = 0.04$  $T_0 = 0.04$
Figure 10. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Cassonian: $H = 0.01$  \hspace{1cm} $\tau_0 = 0.08$

$R_X = 1.0$  \hspace{1cm} $R_Y = 0.001$
Figure 11. Contours of Stream Function (\(\psi\)) and Shear Stress (\(\tau_{yx}\))

Cassonian: \(H = 0.01\)
\(R = 1.0\)
\(\tau_0 = 0.2\)
\(R_y = 0.001\)
Figure 12. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$

Cassonian: $H = 0.01$, $\tau_0 = 0$

$R_x = 1.0$, $R_y = 0.001$
Figure 13. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$

Cassonian: $H = 0.01$  \quad $\tau_0 = 0.01$

$R_x = 1.0$  \quad $R_y = 0.001$
Figure 14. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs Y.

Cassonian: $H = 0.01 \quad \tau_0 = 0.04$

$R_x = 1.0 \quad R_y = 0.001$
Figure 15. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Cassonian: $H = 0.01 \quad \tau_o = 0.08$

$R_x = 1.0 \quad R_y = 0.001$
Figure 16. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Cassonian: $H = 0.01$ \hspace{1cm} $\tau_0 = 0.2$

$R_x = 1.0$ \hspace{1cm} $R_y = 0.001$
(3) The velocity component in the X direction \( (V_x) \) is plotted against Y in Figures 17 through 21. It can be seen that the plug flow close to the center plane becomes more prominent as the value of the finite yield stress term \( \tau_0 \) increases. When \( \tau_0 \) is set equal to zero in Figure 17, the flow becomes Newtonian and there is no plug flow. The maximum dimensionless velocity \( (V_x)_{\text{max}} \), which is \( (v_x)_{\text{max}}/U_0 \), equals 1.5 as predicted for Newtonian flow.

(4) The pressure on the central plane is plotted against X in Figure 22. It can be seen that the existence of a finite yield stress causes greater pressure drop.

**Effect of Wall Suction Rate \( (R_y) \)**

The effect of wall suction on the flow was studied by changing the value of the wall Reynolds number \( R_y \) while holding the other variables constant. The half distance between the two parallel membranes was again 0.01 cm. The entrance Reynolds number \( (R_x) \) was 1.0 and the yield stress \( \tau_0 \) was 0.04 dyne/cm\(^2\). The wall Reynolds numbers were 0, 0.00025, 0.0005, 0.00075, 0.001, 0.0015 and 0.002. The results are presented in the following groups of plots:

(1) The contours of the stream function \( (\psi) \) and the shear stress are presented in Figures 23 through 29. When \( R_y \) is zero, the flow is reduced to one-dimensional. The stream function \( (\psi) \) and shear stress \( (T_{yx}) \) are independent of the value of X and the contours of both the stream function \( (\psi) \) and the shear stress go straight through the channel. When there is a suction on the wall, both the stream function and the
Figure 17. Velocity Profiles ($V_x$).

Cassonian: $H = 0.01$, $\tau_0 = 0$, $R_x = 1.0$, $R_y = 0.001$
Figure 18. Velocity Profiles ($V_x$).

Cassonian: $H = 0.01 \quad \tau_0 = 0.01$

$R_x = 1.0 \quad R_y = 0.01$
Figure 19. Velocity Profiles ($V_x$).

Cassonian: $H = 0.01 \quad \tau_0 = 0.04 \quad R_x = 1.0 \quad R_y = 0.001$
Figure 20. Velocity Profiles ($V_x$).

Cassonian: $H = 0.01 \quad \tau_0 = 0.08$

$R_x = 0.0 \quad R_y = 0.001$
Figure 21. Velocity Profiles \((V_X)\).

Cassonian: \(H = 0.001\)  \(\tau_0 = 0.2\)

\(R_X = 1.0\)  \(R_Y = 0.001\)
Figure 22. Pressure on the Central Plane vs. $X$

$H = 0.01$, $R_x = 1.0$, $R_y = 0.001$
Figure 23. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Cassonian: $H = 0.01$, $\tau_0 = 0.04$

$R_x = 1.0$, $R_y = 0$
Figure 24. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Cassonian: $H = 0.01 \quad \tau_0 = 0.04$

$R_x = 1.0 \quad R_y = 0.00025$
Figure 25. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Cassonian: $H = 0.01$, $\tau_0 = 0.04$

$R_x = 1.0$, $R_y = 0.0005$
Figure 26. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Cassonian:  $H = 0.01$  \quad  $\tau_0 = 0.04$  \\
\quad  $R_x = 1.0$  \quad  $R_y = 0.00075$
Figure 27. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Cassonian: $H = 0.01$ \hspace{1cm} $\tau_0 = 0.04$

$R_x = 1.0$ \hspace{1cm} $R_y = 0.001$
Figure 28. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$)

Cassonian: $H = 0.01$  \hspace{1cm} $\tau_0 = 0.04$

$R_x = 1.0$  \hspace{1cm} $R_y = 0.0015$
Figure 29. Contours of Stream Function ($\psi$) and Shear Stress ($T_{yx}$).

Cassonian: $H = 0.01$, $\tau_0 = 0.04$

$R_x = 1.0$, $R_y = 0.002$
shear stress decrease with increasing $X$ and the contours start to end into the walls. The larger the wall suction, the faster the stream function and shear stress decrease with increasing $X$ and the greater the number of contours that end into the walls. This agrees with what would have been logically expected.

(2) The stream function ($\psi$) and shear stress ($T_{yx}$) vs $Y$ at four suction rates ($R_y = 0, 0.0005, 0.001$ and $0.002$) are presented in Figures 30 through 33. Plots of Newtonian flow for the same $R_x$ and $R_y$ values are presented in Figures 34 through 37 for comparison. In Figure 30 when there is no wall suction ($R_y = 0$), the stream functions at different values of $X$ fall on the same curve and so do the shear stress values. When there is wall suction, the stream function and shear stress have different values at different $X$ values. The larger the suction rate, the wider the curves separate from each other because of the decrease in stream function values and shear stress values. The effect of suction rate are similar in Cassonian and Newtonian flow. The only difference is that the Cassonian flow has larger shear stress values than the Newtonian flow with the same $R_x$ and $R_y$ values.

(3) The velocity profiles of $V_x$ at $X = 0, 20, 40, 60, 80, 100$ were calculated from the stream function values and the results are presented in Figures 38 through 41. $V_x$ decreases with increasing $X$ and the rate of decrease is greater with greater wall suction.

(4) The velocity profiles of $V_y$ at $X = 0, 20, 40, 60, 80, 100$ were calculated from the stream function values and the results are presented in Figures 42 through 45. The $Y$-component of velocity, $V_y$,
Figure 30. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Cassonian: $H = 0.01 \quad \tau_0 = 0.04$

$R_x = 1.0 \quad R_y = 0$
Figure 31. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $y$.

Cassonian: $H = 0.01 \quad \tau_o = 0.04$

$R_x = 1.0 \quad R_y = 0.0005$
Figure 32. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Cassonian: $H = 0.01$ \hspace{1cm} $T_o = 0.04$

$R_x = 1.0$ \hspace{1cm} $R_y = 0.001$
Figure 33. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Cassonian: $H = 0.01$ \hspace{1cm} $\tau_0 = 0.04$

$R_x = 1.0$ \hspace{1cm} $R_y = 0.002$
Figure 34. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Newtonian: $H = 0.01$

$R_x = 1.0$

$R_y = 0$
Figure 35. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Newtonian: $H = 0.01$

$R_x = 1.0$

$R_y = 0.0005$
Figure 36. Stream Function ($\psi$) and Shear Stress ($\tau_{yx}$) vs $Y$.

Newtonian: $H = 0.01$

$R_x = 1.0$

$R_y = 0.001$
Figure 37. Stream Function (ψ) and Shear Stress (∇yX) vs Y.

Newtonian: \[ H = 0.01 \]

\[ R_x = 1.0 \]

\[ R_y = 0.002 \]
Figure 38. Velocity Profiles ($V_x$):
Cassonian: $H = 0.01$, $T_0 = 0.04$, $R_x = 1.0$, $R_y = 0$

$x = 0, 20, 40, 60, 80, 100$
Figure 39. Velocity Profiles ($V_x$).

Cassonian: $H = 0.01 \quad \tau_o = 0.04$

$R_x = 1.0 \quad R_y = 0.0005$
Figure 40. Velocity Profiles ($V_x$).

Cassonian: $H = 0.001$, $\tau_0 = 0.04$

$R_X = 1.0$, $R_Y = 0.001$
Figure 41. Velocity Profiles ($V_x$).

Cassonian: $H = 0.01$, $\tau_0 = 0.04$, $R_x = 1.0$, $R_y = 0.002$.
Figure 42. Velocity Profile ($V_y$).

Cassonian: $H = 0.01$, $\tau_0 = 0.04$

$R_x = 1.0$, $R_y = 0.0005$
Figure 43. Velocity Profile ($V_y$).

Cassonian: $H = 0.01$, $\gamma_0 = 0.04$, $R_x = 1.0$, $R_y = 0.001$
Figure 44. Velocity Profile ($V_y$).

Cassonian: $H = 0.01$ \quad $\tau_o = 0.04$

$R_x = 1.0$ \quad $R_y = 0.002$
Figure 45. Pressure Drop on the Central Plane vs $X$.

Cassonian: $H = 0.01 \quad \tau_0 = 0.04 \quad R_x = 1.0$
Figure 46. Pressure Drop on the Central Plane vs X.

Comparison: $H = 0.01$, $\tau_0 = 0.04$, $R_x = 1.0$
arises as a result of wall suction. When there is no wall suction, 
\( V_y = 0 \) and \( R_y = 0 \) and there is no velocity profile of \( V_y \). Therefore 
there is no curve shown in the plot where \( R_y = 0 \) and this plot is omitted. 
With constant wall suction, the velocity profiles of \( V_y \) are essentially 
the same at different \( X \) values and the computer plotter traced the 
same curves six times in each plot.

(5) The pressure drop on the central plane is plotted in Figure 45. The pressure drop follows a straight line with no wall suction 
\( (R_y = 0) \). The pressure drop becomes smaller and follows a curved line 
when there is a wall suction. Pressure drops of Newtonian flow with the 
same \( R_x \) and \( R_y \) are plotted as dotted lines in Figures 46. Cassonian 
flow (solid lines) has larger pressure drops than Newtonian flow.

Some Mutually Related Variables

Newtonian Flow:

For Newtonian flow:

\[
\psi' = \left[ \frac{3}{2} \frac{V_y}{H} - \frac{1}{2} \left(\frac{V_y}{H}\right)^3 \right] (V_o x - \frac{Q_0}{W}) \tag{4-1}
\]

where

\[
v_x = -\frac{3\psi'}{2y}, \quad v_y = \frac{3\psi'}{2x}
\]

\[
\tau_{yx} = \frac{3uv}{H^3} \left( \frac{1}{2} \frac{Q_0}{W} - v_o x \right) \tag{4-2}
\]

Let \( X = x/H, \quad Y = y/H, \quad \psi = -\psi' W/Q_0, \quad U_o = Q_o/2WH \)

\[
R_x = 4U_o H \rho / u, \quad R_y = v_o H \rho / u, \quad \tau_{yx} = \tau_{yx} / oU_o^2
\]

then the above equations can be written in the dimensionless form
\[ \psi = \left( \frac{3}{2} Y - \frac{1}{2} Y^3 \right) \left( 1 - 2 \frac{R_y}{R_x} X \right) \]  
(4-3)

\[ T_{yx} = \frac{12}{R_x} Y \left( 1 - 4 \frac{R_y}{R_x} \right) \]  
(4-4)

From equations (4-3) and (4-4) it can be seen that as long as we keep the ratio of \( R_y/R_x \) the same, the dimensionless stream function \( \psi \) will always stay the same and the dimensionless shear stress will change inversely with \( R_x \). The distance between the membranes has no effect either on the dimensionless stream function \( \psi \) or on the dimensionless shear stress \( T_{yx} \). This has been tested numerically and the results are plotted in Figures 47 through 53.

Use Figure 47 as the base case with \( H = 0.01, R_x = 1.0 \) and \( R_y = 0.001 \). \( H \) was changed to 0.05 in Figure 48 and to 0.005 in Figure 49. The plots remain unchanged, proving that the value of \( H \) has no effect on \( \psi \) or \( T_{yx} \). In Figure 50, \( R_x \) and \( R_y \) are changed to 25 and 0.025 respectively. The resulting plots have the same \( \psi \) values but the \( T_{yx} \) values become much smaller. If these \( T_{yx} \) values are multiplied by \( R_x \) as shown in Figure 51, the plot becomes the same as that in Figure 47 again. In Figure 52, \( R_x \) and \( R_y \) are changed to 0.25 and 0.00025 respectively. The resulting plot again has the same \( \psi \) values but the \( T_{yx} \) values become much greater. If these \( T_{yx} \) values are multiplied by \( R_x \) as in Figure 53, the plot again becomes the same as that in Figure 47.

Cassonian Flow:

The flow equations for a Cassonian flow can be written as:
Figure 47. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs Y.

Newtonian: $H = 0.01$

$R_x = 1.0$

$R_y = .001$
Figure 48. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$

Newtonian: $H = 0.05$

$R_x = 1.0$

$R_y = 0.001$
Figure 49. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Newtonian: $H = 0.005$

$R_x = 1.0$

$R_y = 0.001$
Figure 50. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs Y

Newtonian: $H = 0.01$

$R_x = 25$

$R_y = 0.025$
Figure 51. Stream Function ($\psi$) and Shear Stress ($T_{yx}$)($R_x$) vs $Y$.

Newtonian: $H = 0.01$

$R_x = 25$

$R_y = 0.025$
Figure 52. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs Y.

Newtonian: $H = 0.01$

$R_x = 0.25$

$R_y = 0.00025$
Figure 53. Stream Function ($\psi$) and Shear Stress ($T_{yx}(R_x)$) vs $Y$.

Newtonian: $H = 0.01$

$R_x = 0.25$

$R_y = 0.00025$
\[ 2F^2(\tau T_y) + D^2 T_y = 0 \]  
(4-4)

where

\[
T_{yx} = -\frac{4}{R_x} \left[ \frac{4H^2}{k^4} \left( \frac{\tau_0}{R_x} \right) \left[ 4(F^2\psi)^2 + (D^2\psi)^2 \right]^{-\frac{1}{4}} \right. \\
\left. + \frac{4D^2H}{k^2} \left( \frac{\tau_0}{R_x} \right) \left[ 4(F^2\psi)^2 + (D^2\psi)^2 \right]^{-\frac{1}{4}} \right]
\]
(4-5)

at \( Y = 0 \), \( \psi = 0 \), \( T_{yx} = 0 \)

at \( Y = 1 \), \( \psi = 1 - V_o X \)

\[
= 1 - \frac{V_o}{U_o} X \\
= 1 - \frac{4R_y}{R_x}
\]

From the above equations and boundary conditions it can be observed that if \( R_x \) and \( R_y \) are kept constant and if the resultant value of the group \( (\rho H^2 \tau_0 / k^4) \) remains the same, equations (4-4) and (4-5) should always have the same solution. If \( (R_y/R_x) \) and \( (\tau_0/R_x) \) are kept the same with \( (\rho H^2 / k^4) \) remaining constant, the value of \( T_{yx} \) will change inversely with \( R_x \). These observations are proved numerically and the results are presented in Figures 54 through 59. In Figure 32, Figure 54 and Figure 55 only H and \( \tau_0 \) have been changed and \( (H^2 \tau_0) = 0.000004 \)
Figure 54. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Cassonian: $H = 0.05$  \hspace{1cm} $\tau_o = 0.0016$

$R_x = 1.0$  \hspace{1cm} $R_y = 0.001$
Figure 55. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Cassonian: $H = 0.005 \quad \tau_0 = 0.16$

$R_x = 1.0 \quad R_y = 0.001$
Figure 56. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Cassonian: $H = 0.01$ $\quad \tau_0 = 1.0$

$R_x = 25$ $\quad R_y = 0.025$
Figure 57. Stream Function (ψ) and Shear Stress (T_{yx})(R_x) vs Y.

Cassonian: \( H = 0.01 \) \( \tau_0 = 1.0 \)
\( R_x = 25.0 \) \( R_y = 0.025 \)
Figure 58. Stream Function ($\psi$) and Shear Stress ($T_{yx}$) vs $Y$.

Cassonian: $H = 0.01$  \hspace{1cm} $\tau_o = 0.01$

$R_x = 0.25$ \hspace{1cm} $R_y = 0.00025$
Figure 59. Stream Function ($\psi$) and Shear Stress ($T_{yx}$)($R_x$) vs $Y$.

Cassonian: $H = 0.01$ \quad $\tau_o = 0.01$

$R_x = 0.25$ \quad $R_y = 0.00025$
in all three cases. The plots turn out to be exactly the same. Now compare Figure 32 and Figure 56. The values that are different are \( \tau_0, R_x \) and \( R_y \). However the values of the ratio \( (R_y/R_x) \) and \( (\tau_0/R_x) \) remain the same at 0.001 and 40 respectively. The resulting plots have the same stream function values but \( T_{yx} \) has much smaller values in Figure 56 than in Figure 32. After multiplying \( T_{yx} \) in Figure 57 by \( R_x \) as shown in Figure 57, the plot becomes the same as that in Figure 32. In Figure 58, the values of the ratio of \( (R_y/R_x) \) and \( (\tau_0/R_x) \) still remain the same but the values of \( \tau_0, R_x \) and \( R_y \) are all much smaller than before resulting in large \( T_{yx} \) values. After multiplying \( T_{yx} \) by \( R_x \) as shown in Figure 59, the plot in Figure 59 again becomes the same as that in Figure 32.

The relations derived above can be used to predict the flow behavior at other conditions from the results of a known condition.
CHAPTER V

CONCLUSIONS AND RECOMMENDATIONS

A new method has been developed in this study to solve the two-dimensional Cassonian flow problem between two parallel permeable membranes. The method consists of reducing the four stress components to one stress component and then introducing a stream function in the simplified equation. The results of the numerical solution are (1) the existence of a finite yield stress in the fluid increases the internal stresses and also increases the pressure drop, (2) the increase in wall suction decreases the internal stress and the pressure drop in the x-direction significantly while producing only a slight increase in the pressure drop in the y-direction which is approximately 1/1000 of the magnitude of the pressure drop in the x-direction, (3) the dimensionless stream function $\psi$ and shear stress $T_{yx}$ remain constant with respect to X when there is no wall flux, and decrease with increasing X values when there is a wall suction.

The method developed here is not limited to rectangular coordinates. It can also be applied to cylindrical and spherical coordinates. The correlations between different stress terms can be derived from the equations of continuity. This technique can also be applied to solve two-dimensional flow problems of other non-Newtonian fluids such as Bingham fluids, Ostwald de Waele fluids, etc.

Recommendations for the extension of this study are:

1. Change the constant wall suction rate to variable wall suction rates.
2. Change the geometry from rectangular to cylindrical to simulate blood ultrafiltration in hollow-fiber membranes.

3. Take into consideration the change in fluid rheological properties with the removal of the ultrafiltrate.
APPENDIX A

CASSONIAN FLOW BETWEEN TWO PARALLEL NON-PERMEABLE PLATES

For steady laminar flow of any fluid between two parallel plates, the shear stress equation is

$$\tau_{yx} = \left(\frac{P_0 - P_L}{L}\right)y$$  \hspace{1cm} (A-1)

For a Cassonian fluid, the shear stress — shear rate relationship is

$$\tau_{yx} = \tau_0 \frac{1}{2} + k\left(-\frac{dv_x}{dy}\right)^{\frac{1}{2}}$$ \hspace{1cm} (A-2)

Taking the square root of equation (A-1) gives

$$\tau_{yx}^{\frac{1}{2}} = \left(\frac{P_0 - P_L}{L}\right)^{\frac{1}{2}} \sqrt{y}$$ \hspace{1cm} (A-3)

Since the flow is symmetrical across the central plane, only the half of the flow field when $y$ is positive is considered. Therefore the negative root has been dropped because $\tau_{yx}$ will always be positive when $y$ is positive. Combining equations (A-2) and (A-3) gives

$$\tau_0 \frac{1}{2} + k\left(-\frac{dv_x}{dy}\right)^{\frac{1}{2}} = \left(\frac{P_0 - P_L}{L}\right)^{\frac{1}{2}} \sqrt{y} \frac{1}{2}$$
Rearranging

\[-\frac{dv_x}{dy} = \frac{1}{k} \left[ \left( \frac{p_o - p_l}{L} \right) \frac{y}{2} - r_0 \right] \]

\[-\frac{dv_y}{dy} = \frac{1}{k^2} \left[ \left( \frac{p_o - p_l}{L} \right) y - 2 \left( \frac{p_o - p_l}{L} \right) r_0 \right] y^{3/2} + r_0 \]

Integrating

\[-v_x = \frac{1}{k^2} \left[ \left( \frac{p_o - p_l}{L} \right) \frac{y^2}{2} - \frac{4}{3} \left( \frac{p_o - p_l}{L} \right) r_0 y^{3/2} + r_0 y \right] + C\]

At \( y = H \), \( v_x = 0 \)

\[C = -\frac{1}{k^2} \left[ \left( \frac{p_o - p_l}{L} \right) H^2 - \frac{4}{3} \left( \frac{p_o - p_l}{L} \right) r_0 H^{3/2} \right] \]

\[+ r_0 H \]

\[v_x = \frac{1}{k^2} \left[ \left( \frac{p_o - p_l}{L} \right) \frac{y^2}{2} - \frac{4}{3} \left( \frac{p_o - p_l}{L} \right) r_0 y^{3/2} + r_0 y \right] \]

\[+ r_0 H \left( 1 - \frac{y}{H} \right) \]  

\[0_o = 2W \int_0^H v_x dy \]

\[= \frac{2WH}{k^2} \left[ \frac{H^2}{2} \left( \frac{p_o - p_l}{L} \right) - \frac{4}{5} \left( \frac{p_o - p_l}{L} \right) r_0 H^{3/2} \right] \]

\[= \frac{2WH}{k^2} \left[ \frac{H}{2} \left( \frac{p_o - p_l}{L} \right) - \frac{4}{5} \left( \frac{p_o - p_l}{L} \right) r_0 \right] \]

\[= \frac{2WH}{k^2} \left[ \frac{H}{2} \left( \frac{p_o - p_l}{L} \right) - \frac{4}{5} \left( \frac{p_o - p_l}{L} \right) r_0 + \frac{r_0 H}{2} \right] \]
where

\[ p_f = \frac{p_o - p_l}{L} \]  \hspace{1cm} (A-6)

Solving equation (A-5) for \( p_f \), we get:

\[ p_f = \frac{6}{5} \left( \frac{\tau_0}{H} \right)^{\frac{3}{2}} + \left( \frac{30 \cdot k^2}{2WH^3} - \frac{3 \tau_0}{50 H} \right)^{\frac{3}{2}} \]  \hspace{1cm} (A-7)

Equations (A-5) and (A-7) can be written in dimensionless variables as

\[ V_x = \frac{1}{K^2} \left( \frac{1}{2} p_f (1 - Y^2) - \frac{4}{3} T_0^{1/2} p_f^{1/2} (1 - Y^{3/2}) + T_0 (1 - Y) \right) \]  \hspace{1cm} (A-8)

where

\[ p_f = \frac{6}{5} T_0^{1/2} + (3k^2 - \frac{3}{50} T_0)^{1/2} \]  \hspace{1cm} (A-9)

\[ p_f = p_f \left( \frac{-H}{\rho U_0} \right) \]

\[ K^2 = \frac{k^2}{\rho U_0 H} \]

Defining

\[ V_x = \frac{\partial \psi}{\partial Y}, \hspace{1cm} V_y = -\frac{\partial \psi}{\partial X} \]

\[ \psi = \int V_x \, dY + C \]

\[ = \frac{V}{K} \left( \frac{1}{2} p_f (1 - Y^2) - \frac{4}{3} T_0^{1/2} p_f^{1/2} (1 - \frac{2}{5} Y^{3/2}) \right. \]

\[ + \left. T_0 (1 - \frac{Y}{2}) \right] + C \]
At $Y = 0$, \[ \psi = 0 \]
\[ C = 0 \]

\[ \psi = \frac{Y}{K^2} \left[ \frac{1}{2} P_f (1 - \frac{Y^2}{3}) - \frac{4}{3} T_0^{\frac{3}{2}} P_f^{\frac{1}{2}} \left(1 - \frac{2}{5} Y^{3/2}\right) \right] + T_0 (1 - \frac{Y}{2}) \]  

(A-10)

Equation (A-1) can also be written in terms of dimensionless variables as

\[ T_{yx} = P_f Y \]  

(A-11)
APPENDIX B

COMPUTER PROGRAMS

The computer programs used in this study are presented here together with a simple logic flow diagram of the main program and definitions of some of the more important symbols used. All programs are written in Fortran IV extended language.

<table>
<thead>
<tr>
<th>Program Symbol</th>
<th>Definition</th>
</tr>
</thead>
<tbody>
<tr>
<td>AN, N</td>
<td>Number of interior grid points in the Y direction.</td>
</tr>
<tr>
<td>ALPHA, BETA</td>
<td>Relaxation factors $\alpha$ and $\beta$.</td>
</tr>
<tr>
<td>AK</td>
<td>Square root of ultimate viscosity coefficient $k$ in Casson equation.</td>
</tr>
<tr>
<td>DUMMY</td>
<td>Temporary print out storage.</td>
</tr>
<tr>
<td>DY</td>
<td>Step size in Y direction, $\Delta Y$.</td>
</tr>
<tr>
<td>D2</td>
<td>$D^2 \psi, \left(\frac{\partial^2 \psi}{\partial Y^2} - \frac{\partial^2 \psi}{\partial \lambda^2}\right)$</td>
</tr>
<tr>
<td>F</td>
<td>Function used in Newton iteration.</td>
</tr>
<tr>
<td>FP</td>
<td>$\frac{\partial F}{\partial \psi_{I+1,J}}$</td>
</tr>
<tr>
<td>F2</td>
<td>$F^2 \psi, \frac{\partial^2 \psi}{\partial \lambda \partial Y}$</td>
</tr>
<tr>
<td>GAMMA</td>
<td>$\gamma, F^2 \psi/D^2 \psi$</td>
</tr>
<tr>
<td>GROUP</td>
<td>$4(F^2 \psi)^2 + (D^2 \psi)^2$.</td>
</tr>
<tr>
<td>H</td>
<td>Half distance between the two parallel membranes.</td>
</tr>
<tr>
<td>I,J</td>
<td>Grid point subscripts in X- and Y-directions.</td>
</tr>
<tr>
<td>Symbol</td>
<td>Description</td>
</tr>
<tr>
<td>----------</td>
<td>-----------------------------------------------------------------------------</td>
</tr>
<tr>
<td>L</td>
<td>Number of grids in X-direction.</td>
</tr>
<tr>
<td>LOOPM</td>
<td>Maximum number of $\psi_i$ iteration loops allowed before terminating the run.</td>
</tr>
<tr>
<td>MXORLP</td>
<td>Maximum number of loops allowed for the iteration of the first line.</td>
</tr>
<tr>
<td>MXSTEP</td>
<td>Maximum number of Newton iteration steps allowed.</td>
</tr>
<tr>
<td>P</td>
<td>Fluid pressure factor, $P_f$.</td>
</tr>
<tr>
<td>PSI</td>
<td>Stream function, $\psi$.</td>
</tr>
<tr>
<td>PSIMAX</td>
<td>Convergence criterion for the stream function.</td>
</tr>
<tr>
<td>QO</td>
<td>Initial volumetric flowrate, $Q_0$.</td>
</tr>
<tr>
<td>RENX</td>
<td>Entrance Reynolds number, $R_X$.</td>
</tr>
<tr>
<td>RENY</td>
<td>Wall Reynolds number, $R_Y$.</td>
</tr>
<tr>
<td>RHO</td>
<td>Fluid density, $\rho$.</td>
</tr>
<tr>
<td>RV</td>
<td>Dimensionless ultimate viscosity coefficient, $K$.</td>
</tr>
<tr>
<td>S</td>
<td>Grid step size ratio, $\Delta X/\Delta Y$.</td>
</tr>
<tr>
<td>SIMAX</td>
<td>Convergence criterion for Newton iteration and False Position iteration.</td>
</tr>
<tr>
<td>TAU</td>
<td>Shear stress, $T_{yx}$.</td>
</tr>
<tr>
<td>TAUO</td>
<td>Yield stress of the fluid, $\tau_0$.</td>
</tr>
<tr>
<td>TAUP</td>
<td>Temporarily stored shear stress.</td>
</tr>
<tr>
<td>TAUMAX</td>
<td>Convergence criterion for the shear stress.</td>
</tr>
<tr>
<td>UO</td>
<td>Average entrance velocity, $U_0$.</td>
</tr>
<tr>
<td>VO</td>
<td>Wall suction velocity, $V_0$.</td>
</tr>
<tr>
<td>VX</td>
<td>Velocity component in the $X$-direction.</td>
</tr>
<tr>
<td>VY</td>
<td>Velocity component in the $Y$-direction.</td>
</tr>
</tbody>
</table>
Start

Read in options and limits

Read in Problem data

Calculate initial values and boundary conditions

Make a first estimate of $\psi_{i,j}$

Make a first estimate of $T_{i,j}$

Calculate $\psi_{i,j}$ on the first line with Newton Iteration

Reset $\psi_{i,j}$ to new values

Is the change in $\psi_{i,j} < \text{SIMAX}$?

Calculate all $\psi_{i,j}$ with (3-23) iteration process

Calculate all $T_{i,j}$ with (3-17)

Is the change in $\psi_{i,j} < \text{PSIMAX}$ and $T_{i,j} < \text{TAUMAX}$?

Set $\psi_{i,j}$ and $T_{i,j}$ to new values

Calculate $V_x, V_y$ and $P$

Make a correction of $T_{i,j}$ on the wall

Plot results

End
TWO-DIMENSIONAL CASSONIAN FLOW PROGRAM

N. WEI (JULY, 1975)

DOUBLE PRECISION PSI, TAU, TAU2, PSIN, PSIN2, PSI2, PSI3, D21, GROUP1, FPSI, D22, GROUP2, FPSI, GAMMA, TAU, U0, PF

DIMENSION PSI(104,33), TAU2(104,33), F2(104,33), TAU3(33),
  NAME(25), GAMMA(104,33), D2(104,33),
  YR(33), XR(104), FPSI(104,33), TAU1(104,33),
  PSIN(104), PSIN2(104), DUMMY(33)

***100** READ INPUT INFORMATIONS *****

***** READ IN PROBLEM IDENTIFICATION CARD *****

101 READ (5,4001) IEND, (NAME(I), I=1,25)

IF (IEND .NE. 0) GO TO 103
WRITE (10,4012)
WRITE (6,4022)
WRITE (6,4002)
WRITE (6,4023)
WRITE (6,4064)
GO TO 9999

***** READ IN OPTIONS *****

103 READ (5,4006) IFTAPE, IFSTEP, ISTEP, INCOLM, INCLIN

***** READ IN CONTROL LIMITS *****

READ (5,4006) SIMAX, MXSTEP, MXORLP, PSIAX, TAUMAX, LOOPM

***** READ IN PROBLEM DATA *****

READ (5,4006) RHO, TAU0, AK, H, REMX, RENY, N, L, S, ALPHA, BETA, LOOPP, LOOPT, ALPHAI, BETAI

***** PRINT PROGRAM NAME, PROBLEM NAME, AND INPUT DATA *****

WRITE (6,4007)
WRITE (6,4008)
WRITE (6,4009) (NAME(I), I=1,25)
GO = REMX*AK/(2.*RHO)
VO = RENY*AK/(H*RHO)
U0 = GO/(2.*H)
WRITE (6,4009) IFTAPE, IFSTEP, ISTEP, INCOLM, INCLIN, SIMAX, MXSTEP, MXORLP, PSIAX, TAUMAX, LOOPM,
WRITE (6,4010) RHO, TAU0, AK, H, GO, VO, REMX, RENY, N, L, S,
  ALPHAI, BETA, LOOPP, LOOPT, ALPHAI, BETAI

*****200** CALCULATE DIMENSIONLESS VARIABLES *****

TAU0 = TAU0/(RHO*U0*U0)
EV = AK/SQRT(RHO*U0*H)
VO = VO/U0
PF = 1.2*SQRT(TAU0) + SQRT(3.*EV*EV - 0.6*TAU0)
WRITE (6,4015) TAU0, EV, VO, PF, U0
C

****300**  CALCULATE INITIAL VALUES  ****

L1 = L - 1
N1 = N + 1
N2 = N + 2
N3 = N + 3
N4 = N + 4
AN = N

DY = 1./(AN + 1.)
DO 310 J = 2, N4
   AJ = J - 2
   Y = DY*AJ
   YR(J) = Y
   PSI(3+J) = Y*(.5*PF*PF*(1. - Y**Y/3.) - TAU0*(1. - .5*Y))/(RV*RV)
   TAU(J) = PF*PF*Y
310 CONTINUE

C

****400**  MAKE A FIRST ESTIMATION OF PSI(I,J)  ****

DO 410 I = 1, L
   AI = I - 3
   X = S*DY*AI
   XR(I) = X
   PSI(I,N3) = 1. - VO*X
   PSI(I,J) = PSI(3,J)*PSI(I,N3)/PSI(3,N3)
410 CONTINUE

C

****500**  MAKE A FIRST ESTIMATION OF TAU(I,J)  ****

DO 510 I = 2, L1
   F2(I,N3) = (PSI(I+1,N4) + PSI(I-1,N2) - PSI(I-1,N4))/((S*S*DY*DY)
   D2(I,N3) = (S*S*PSI(I,N4) + PSI(I,N3)) - 2.*(S*S-1.)*PSI(I,N3)
   GROUP = 4.*F2(I,N3)***2 + D2(I,N3)***2
   IF (GROUP .LT. 1.E-20) GROUP = 1.E-20
   TAU(I,N3) = - (TAU0/SORT(GROUP) + 2.*SORT(TAU0)*RV/RV*GROUP**.25
   + RV*RV)*D2(I,N3)
510 CONTINUE

C

PSIN2 = PSI(4,N2)
PSIN4 = PSI(4,N4)

C

****600**  CALCULATE (PSI) ON THE FIRST LINE  ****

J0AL = 0
I = 4
6C2 5AN = 9
DO 610 J = 3, N2
   JUST = 0
   KSTEP = 0
   MUNE = 1
   SHIFT = 1*
   PSI5(4,J) = PSI(4,J)
610 CONTINUE
604 \text{PSI}(4, J) = \text{PSI}(4, J+1) + \text{PSI}(2, J-1) - \text{PSI}(4, J-1)
\text{F2}(3, J) = \frac{1}{(4*S*DY*DY)} \text{PSI}(2, J+1)/((4*S*DY*DY)
\text{D2}(3, J) = (S*S*(\text{PSI}(3, J+1) + \text{PSI}(3, J-1)) - 2*(S*S-1)*\text{PSI}(3, J)
\text{GROUP} = 4*F2(3, J)+2 + D2(3, J)*2

F = (TAU0/SCRT(GROUP)) + 2*SCRT(TAU0)*R/V/GROUP**1.25

FP = (TAU0/SCRT(GROUP)**1.5) + SCRT(TAU0)*R/V/GROUP**1.25)*

1 = \text{D2}(3, J)**2/(S*S*DY*DY) - (TAU0/SCRT(GROUP))
2 = 2*SCRT(TAU0)*R/V/GROUP**25 + RV*R/V)/(S*S*DY*DY)

IF (ABS(F) >= TOL, 15,) GO TO 609

IF (JUST < 0.0) GO TO 605

WRITE (6,4011) J, JORL, MOVE, NSTEP, PSI(4, J), F

605 \text{PSI}(4, J) = \text{PSI}(4, J+1) = \text{PSI}(4, J)

IF (ABS(PSI(4, J)) <= SIMAX) GO TO 609

IF (NSTEP < GT, NSTEP) GO TO 606

NSTEP = NSTEP + 1

GO TO 604

606 IF (MOVE < GT, 20) GO TO 607

MOVE = MOVE + 1

FN = MOVE/2

SHIFT = - SHIFT

PSI(4, J) = PSI(4, J) + SHIFT*0.7*FN*(PSI(3, J) - \text{PSI}(4, J))

STEP = 0

GO TO 604

607 IF (JUST > 0) GO TO 608

JUST = JUST + 1

PSI(4, J) = PSI(4, J)

MOVE = 1

SHIFT = 1

STEP = 0

GO TO 604

608 WRITE (6,4012) I, J, JORL, PSI(4, J), F

GO TO 101

609 IF (JORL < GT, LOG(10), BETA = \beta_{A1}

PSI(4, J) = PSI(4, J) + \beta_{A1}*(PSI(4, J) - PSI(4, J))

IF (ABS(PSI(4, J)) <= SIMAX) MARK = MARK + 1

610 CONTINUE

IF (MARK = EQ, 0) :0 TO 621

IF (JORL < LT, MAX(R),) GO TO 612

WRITE (6,4013) JORL, MARK

GO TO 101

612 JORL = JORL + 1

IF J = 3, N2

PSI(4, J) = PSI(4, J)

CONTINUE

GO TO 602

621 IF J = 3, N2

PSI(4, J) = PSI(4, J)

CONTINUE

PSI(4, J) = PSI*(4, J) - PSI(4, J) = PSI(N4+1, N2)/PSI(N2)

C

******* ENTER I: TO BIG LOOP *******
C

*******700** RELAXATION OF (PSI) *******
C
LOOP = J

701 PSIT = 0
TAUT = 0
GO 711
I = 4, L1
II = I + 1
PSI(IP+2(I)) = PSI(I-1,N2)
PSI(I+4(I)) = PSI(I-3,N2)
GO 710
J = 3, N2
JUST = 0
NS1EP = 1
MOVE = 0
PSI(I,J) = PSI(I,J)

7011 PSI1 = PSI(I,J)

702 F2(I,J) = PSI(I+1,J+1) + PSI(I-1,J-1) - PSI(I+1,J-1)
           - PSI(I-1,J+1) + PSI(I,J-1) - 2*(S*S - 1.)*PSI(I,J)
1
D2 = (S*S*(PSI(I,J+1) + PSI(I,J-1)) - 2*(S*S - 1.)*PSI(I,J)
1
GROUP1 = 4.*F2(I,J)*2 + D2**2
IF (GROUP1 LT, 1.E-20) GROUP1 = 1.E-20
FPSI1 = (TAU0/SQRT(GROUP1) + 2.*SQRT(TAU0)*RV/GROUP1**.5
1
        + RV/RV)*21 + TAU(I,J)
1
IF (ABS(FPSI1) LT, 1.E-06) GO To 710
PSI2 = 0.

702 F2(I,J) = PSI(I+1,J+1) + PSI(I-1,J-1) - PSI(I+1,J-1)
           - PSI(I-1,J+1) + PSI(I,J-1) - 2*(S*S - 1.)*PSI(I,J)
1
D2 = (S*S*(PSI(I,J+1) + PSI(I,J-1)) - 2*(S*S - 1.)*PSI(I,J)
1
GROUP2 = 4.*F2(I,J)*2 + D2**2
IF (GROUP2 LT, 1.E-20) GROUP2 = 1.E-20
FPSI2 = (TAU0/SQRT(GROUP2) + 2.*SQRT(TAU0)*RV/GROUP2**.5
1
        + RV/RV)*22 + TAU(I,J)
1
IF (FPSI1*FPSI2 LT, 0.) GO TO 703
IF (MOVE GT, 0) GO TO 7021
PSI3 = PSI1
FPSI3 = FPSI1
PSI2 = 1.
MOVE = 1
GO TO 702

7021 FTEST = FPSI3*FPSI3 - FPSI2*FPSI2
IF (FTEST L.T. 0.) GO TO 703
PSI2 = PSI1
FPSI2 = FPSI1

703 PSI1(I,J) = PSI2 - FPSI2*(PSI2-PSI1)/(FPSI2-FPSI1)
           - PSI1(I,J-1) + PSI(I,J-1) - 2*(S*S - 1.)*PSI(I,J)
1
D2 = (S*S*(PSI(I,J+1) + PSI(I,J-1)) - 2*(S*S - 1.)*PSI(I,J)
1
GROUP = 4.*F2(I,J)*2 + D2(I,J)*2
IF (GROUP L.T. 1.E-23) GROUP = 1.E-20
FPSI = (TAU0/SQRT(-GROUP) + 2.*SQRT(TAU0)*RV/GROUP**.5
1
        + RV/RV)*23 + TAU(I,J)
1
IF (GROUP L.E. 0.) GO TO 720
WRITE (6,'(I4,0)') I,J, L00P,NS1EP, PSI1(I,J), FPSI

703 IF (ABS(FPSI1(I,J) -PSI2) LT, SIMAX) GO TO 709
IF (ABS(FPSI2(I,J) -PSI1) LT, SIMAX) GO TO 709
IF (FPSI1*FPSI2 LT, 0.) GO TO 705
IF (FPSI1*FPSI2 LT, 0.) GO TO 705
PSI2 = PSI1(I,J)
FPSI2 = FPSI1
GO TO 706

705 PSI1 = PSI2
FPSI1 = FPSI2
PSI2 = PSI1(I,J)
FPSI2 = FPSI
706 IF (NSTEP .GT. MXS*EP) GO TO 707
NSTEP = NSTEP + 1
GO TO 703

707 IF (JUST .GT. 0) GO TO 708
JU^T = JUST + 1
PSIP(IJ,J) = PSI(IJ,J)
MOVE = 0
NSTEP = 1
GO TO 7011

708 IF (6.4012) IL,J, LOOP, PSIN(IJ,J), FPSI
GO TO 701

709 PSI'T = PSI'T + ABS(PSIP(I,J) - PSI(I,J))
710 CONTINUE

711 CONTINUE

SPSI = 0.
DO 715 I = 5, L
SPSI = SPSI + AN*PSI(I+N3)

715 CONTINUE

PSI'T = PSI'T/SPSI
DO 730 I = 4, L1
I1 = I + 1
PSIP(I1,2) = 0.
PSIP(I1,N3) = PSI(I1,N3)
PSIP(I1,1) = PSIP(I1,3)
PSIP(I1,N4) = PSINN4(I1)*PSIP(I1,N2)/PSINN2(I1)

730 CONTINUE

C
C ***9039*** RELAXATION OF (TAU) ***9***
C
L2 = L - 2
DO 910 I = 2, L1
DO 910 J = 2, M3
F2(I,J) = (PSI(I+1,J+1) + PSI(I-1,J-1) - PSI(I+1,J-1) - PSI(I-1,J+1))/4.*S*DY*DY
D2(I,J) = (S*S*(PSI(I,J+1) + PSI(I,J-1)) - 2.*(S*S-1)*PSI(I,J)
1 - PSI(I,J) - PSI(I-1,J) + PSI(I+1,J))/S*S*DY*DY
IF (ABS(D2(I,J)) .LE. 1.E-20) GA^MA(I,J) = 1.E-20
GAMMA(I,J) = F2(I,J)/D2(I,J)

910 CONTINUE

DO 920 I = 3, L2
I1 = I + 1
DO 920 J = 2, M3
IF (ABS(D2(I+1,J+1)) .LE. 1.E-20) GO TO 913
IF (ABS(D2(I-1,J-1)) .LE. 1.E-20) GO TO 913
IF (ABS(D2(I+1,J-1)) .LE. 1.E-20) GO TO 913
IF (ABS(D2(I-1,J+1)) .LE. 1.E-20) GO TO 913
TAU^D(I,J) = S*S*(TAU(I,J+1) + TAU(I,J-1)) - 2.*(S*S-1)*TAU(I,J)
1 - TAU(I-1,J) - S*(GAMMA(I,J)*TAU(I+1,J+1)
2 + GAMMA(I+1,J-1)*TAU(I+1,J-1) - GAMMA(I+1,J-1)*
3 TAU(I-1,J+1) - GAMMA(I-1,J+1)*TAU(I-1,J+1))

914 CONTINUE

913 TAU^D(I,J) = (TAU(I,J+1) + TAU(I,J-1))/2.
914 TAU^D = TAU^D + ABS(TAU^D(I,J) - TAU(I,J)))

CONTINUE

TAU^D(I,J) = 0.
TAU^D(I,J,N3) = TAU(I,J,N3)

920 CONTINUE

STAU = 0.
DO 930 I = 4, L1
STAU = STAU + AN*TAU(I,N3)

930 CONTINUE
CONTINUE

TAUT = TAUT/STAU
IF (PSIT .LT. PSIMAX .AND. TAUT .LT. TAUMAX) GO TO 982
IF (LOOP .LT. LOOPM) GO TO 931
WRITE (6,*(14)) LOOP, A
GO TO 101
931 IF (LOOP .LT. LOOPM) ALPHA = ALPHA1
IF (LOOP .GT. LOOP, J) BETA = BETA1
DO 944 I = 4, L1
I1 = I + 1
DO 935 J = 3, N2
PSI(I1,J) = PSI(I1,J) + BETA*(PSIP(I1,J) - PSI(I1+1,J))
TAU(I1,J) = TAU(I1,J) + ALPHA*(TAUP(I1,J) - TAU(I1+1,J))
935 CONTINUE
PSI(I1,1) = PSI(I1,1) + BETA*(PSIP(I1,1) - PSI(I1,1))
PSI(I1,N4) = PSI(I1,N4) + BETA*(PSIP(I1,N4) - PSI(I1,N4))
940 CONTINUE

C

****808** MAKE A FIRST CORRECTION OF (TAU) ON WALL ****

DO 940 I = 4, L1
F2(I,N3) = (PSI(I+1,N4) + PSI(I-1,N2) - PSI(I+1,N2) - PSI(I-1,N4))/(4.*S*S)
F2(I,N3) = (PSI(I+1,N4) + PSI(I-1,N2) - 2.*S*S-1.)*PSI(I,N3)
GROUP = 4.*F2(I,N3)**2 + F2(I,N3)**2
IF (GROUP .LT. 1.E-20) GROUP = 1.E-20
TAU(I,N3) = - (TAU/SORT(GROUP) + 2.*SORT(TAU)*RV)/GROUP**.25 + RV*RV)*F2(I,N3)
TAU(I,r) = 0.
940 CONTINUE

C

********** END OF WALL (TAU) CORRECTION **********

LAST = 0
IF (IFSTEP .EQ. 0) GO TO 981
IF (IFSTEP .EQ. LOOP/15+EP) ME, LOOP) GO TO 981
WRITE (6,*(140)) LOOP,
981 DO 945 J = 2, N3
PSIP(3,J) = PSI(3,J)
TAUP(3,J) = TAU(3,J)
945 CONTINUE
PSIP(4,N3) = PSI(4,N3)
NS = N1/INCOLM + 1
DO 950 J = 1, NS
JS = 2 + (J-1)*INCOLM
YPM(Y(J)) = YP(JS)
950 CONTINUE
WRITE (6,*(4015)) (YPM(X), X=1,NS)
DO 960 I = 3, L, INCOLM
AI = 1 - 3
XR(I) = S*DY*AI
DO 960 J = 1, NS
JS = 2 + (J-1)*INCOLM
YPM(Y(J)) = PSIP(I,JS)
960 CONTINUE
WRITE (6,*(4017)) XR(I), (YPM(X), X=1,NS)
DO 970 J = 1, NS
JS = 2 + (J-1)*INCOLM
YPM(Y(J)) = TAUP(I,JS)
970 CONTINUE
WRITE (6,401A) (DIMM(Y,J), J=1,N5)

980 CONTINUE
IF (ITAPE .EQ. 3) GO TO 991
WRITE (16,4021) I3, L, S, DY, TAU, RV, RENX
WRITE (10*402A) (XRC(I), I=1,2,N9)
WRITE (10*4021) (XR(I), I=1,3)
WRITE (10*4024) (PSI(I,J), J=2,N3)
WRITE (10*4022) (YR(I,J), J=2,N3)
DO 990 I = 2, L
AI = I - 3
XR(I) = S*DY*AI
WRITE (10*4021) XR(I)
WRITE (10*4024) (PSI(I,J), J=2,N3)
WRITE (10*4022) (YR(I,J), J=2,N3)
990 CONTINUE
IF (LAST .GT. 0) GO TO 981
LOOP = LOOP + 1
GO TO 971
982 LAST = 99
WRITE (6,4019)
90 TC 941
C
********** FORMAT LIST **********
C
4001 FORMAT (11,4X,15.3,1OA3)
4002 FORMAT (11H//)
4003 FORMAT (11H*,48H END OF PROBLEMS, TEAR OFF THIS PAGE, GOOD LUCK. )
4004 FORMAT (11H1)
4005 FORMAT (1)
4007 FORMAT (11H*,110H TWO DIMENSIONAL CASSONIAN FLOW PROGRAM (I1)
1 JULY, 1975 NAN WEI )
4008 FORMAT (11H* INPUT DATA (1=YES, 0=NO)*/
4009 FORMAT (11H INPUT DATA */
1 WRITE RESULTS ON TAPE = */ I1/
2 LOOP STEP PRINT OUT = */ I1/
3 INCREMENTS IN LOOP STEP PRINT OUT = */ I3/
4 COLUMN INCREMENTS IN PRINT OUT = */ I3/
5 LINE INCREMENTS IN PRINT OUT = */ I3/
6 MAX PSI POINT ITERATIONS = */ IPE12.6/
7 MAX ITERATION STEPS = */ I3/
8 MAX PSI RELAXATION STEPS ON FIRST LINE = */ I3/
9 MAX PSI TOLERANCE = */ IPE12.6/
10 MAX TAU TOLERANCE = */ IPE12.6/
11 MAX PSI-ITAU RELAXATION STEPS = */ I4/
12 MAX PSI-ITAU RELAXATION TOLERANCE = */ IPE12.6/
13 MAX PSI-ITAU RELAXATION TOLERANCE = */ IPE12.6/
14 MAX PSI-ITAU RELAXATION TOLERANCE = */ IPE12.6/
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80 MAX PSI-ITAU RELAXATION TOLERANCE = */ IPE12.6/
**FORMAT LIST**

- **FORM** (1H1, 1PE12.5)  
  **FORMAT** (1H1, 1PE12.6/ 8(3X, 1PE12.6))
- **FORM** (1H1, 1PE12.5)  
  **FORMAT** (1H1, 8(3X, 1PE12.6))
- **FORM** (1H1, 1PE12.5)  
  **FORMAT** (1H1, 8(3X, 1PE12.6))
- **FORM** (1H1, 1PE12.5)  
  **FORMAT** (1H1, 8(3X, 1PE12.6))
- **FORM** (1H1, 1PE12.5)  
  **FORMAT** (1H1, 8(3X, 1PE12.6))
- **FORM** (1H1, 1PE12.5)  
  **FORMAT** (1H1, 8(3X, 1PE12.6))
- **FORM** (1H1, 1PE12.5)  
  **FORMAT** (1H1, 8(3X, 1PE12.6))
- **FORM** (1H1, 1PE12.5)  
  **FORMAT** (1H1, 8(3X, 1PE12.6))
- **FORM** (1H1, 1PE12.5)  
  **FORMAT** (1H1, 8(3X, 1PE12.6))

**RESULTS**

- **LOOP** = 'R
- **TAU** = '1PE12.6/ 8(3X, 1PE12.6))
- **TAU** = '1PE12.6/ 8(3X, 1PE12.6))
- **TAU** = '1PE12.6/ 8(3X, 1PE12.6))
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- **TAU** = '1PE12.6/ 8(3X, 1PE12.6))

**END OF FORMAT LIST**

**END**

**STREAM FUNCTION CHECK OUT PROGRAM**

N. WEI (APRIL 29, 1975)

**DOUBLE PRECISION** PSI(104*64), TAU(104*64), TAUP(104*64), NAME(25), Y(64), P(104*33)

**READ IN DATA CARDS**

101 READ (5, 1001) IEND, (NAME(I), I = 1, 25)
   IF (IEND .GT. 0) GO TO 102
   WRITE (6, 1002)
   WRITE (6, 1002)
   WRITE (6, 1003)
   WRITE (6, 1004)
   GO TO 999
102 READ (5, 1007) ISTYPF, IFREAL, RENX, H, RENY, A, TAU0, AK, RHO, S, D, L, N, INCPRT, IPRT1, IPFLOT
   WRITE (6, 1005)
   WRITE (6, 1005)
   WRITE (6, 1006) (NAME(I), I = 1, 25)
   Q = RENX*AK*AK/(2.*RHO)
   VO = RENY*AK*AK/(H*RHO)
   IF (IPRT1 .EQ. 0) GO TO 301
   WRITE (6, 1008) ISTYPF, IFREAL, 0, RENX, H, VO, RENY, A, TAU0, AK, RHO, S, D, L, N, INCPRT, IPRT1, IPFLOT

**CALCULATE AND PRINT PSI**

301 N4 = N + 4
   N3 = N + 3
   UO = 0/(2.*H)
   RV = AK/SQRT(RHO*UO*H)
   AN = N
   DY = H/(AN+1.)
   DO 310 J = 2, N4
      AJM = J - 2
      Y(J) = DY*AJM
   310 CONTINUE
   DO 330 I = 2, L
      AI = I - 3
      X = S*DY*DI*AI
\[
\begin{align*}
no & 320 \quad J = 2 \times N4 \\
AY & = Y(J) \\
TPSI & = FPSI(X, \ AY, Q*H, VO+A, TAU0+AK, S*ISTYPE) \\
TTAU & = TTAU(X, \ AY, Q*H, VO+A, TAU0+AK, S*ISTYPE) \\
PSI(I,J) & = TPSI*2./Q \\
TAU(I,J) & = TTAU/(RHO*U0*U0) \\
IF (ISTYPE .EQ. 2) \quad GO \ TO \ 320 \\
P(I,J) & = (V0*(X*AX - AY*AY) - Q*X)*1.5*AK*AK/(H**3*RHO*U0*U0) \\
320 & \quad CONTINUE \\
PSI(I,1) & = - PSI(I,3) \\
330 & \quad CONTINUE \\
L1 & = L - 1 \\
CY & = DY/H \\
TAU0 & = TAU0/(RHO*U0*U0) \\
no & 340 \quad I = 2 \times L1 \\
no & 340 \quad J = 2 \times N3 \\
F2 & = (PSI(I+1,J+1) + PSI(I-1,J-1) - PSI(I+1,J-1) - PSI(I-1,J+1)) \\
& \times (S*S*C+CY*CY) \\
D2 & = (S*S*(PSI(I,J+1) + PSI(I,J-1)) - 2*(S*S-S)*PSI(I,J)) \\
& \times (S*1,J-1)/(S*S*C+CY) \\
GROUP & = 4*F2*F2 + D2*D2 \\
IF (GROUP .LT. 1.E-20) \quad GROUP = 1.E-20 \\
TAUP(I,J) & = -(TAU0/SQR(TGROUP)) + 2*SQR(TAU0)*RV/GROUP**.25 \\
& + RV*RV)*D2 \\
340 & \quad CONTINUE \\
YD & = \ H \\
PD & = \ 1. \\
TD & = \ 1. \\
IF (IFREAL .EQ. 0) \quad GO \ TO \ 341 \\
YD & = \ 1. \\
PD & = \ Q/2. \\
TD & = \ RHO*U0*U0 \\
341 & \quad NS = (N + 1)/INCPRT + 1 \\
no & 345 \quad J = 1*NS \\
JS & = 2 + (J-1)*INCPRT \\
Y(J) & = Y(JS)/YD \\
345 & \quad CONTINUE \\
no & 350 \quad I = 2 \times L \\
no & 350 \quad J = 1*NS \\
JS & = 2 + (J-1)*INCPRT \\
PSI(I,J) & = PSI(I,JS)*Pn \\
TAU(I,J) & = TAU(I,JS)*Tn \\
TAUP(I,J) & = TAUP(I,J)*TD \\
P(I,J) & = P(I,JS) \\
350 & \quad CONTINUE \\
WRITE (6, 1009) IFREAL, (Y(J), J = 1*NS) \\
DO & 360 \quad I = 2 \times L \\
AI & = I - 3 \\
X & = S*DY*DAI \\
IF (IFREAL .EQ. 1) \quad GO \ TO \ 353 \\
X & = X/H \\
353 & \quad WRITE (6, 1010) X, (PSI(I,J), J = 1*NS) \\
WRITE (6, 1011) (TAU(I,J), J = 1*NS) \\
WRITE (6, 1012) (PI(I,J), J = 1*NS) \\
WRITE (6, 1013) (TAUP(I,J), J = 1*NS) \\
360 & \quad CONTINUE \\
IF (IFPLOT .EQ. 0) \quad GO \ TO \ 101 \\
WRITE (9, 4011) N3, L, S, DY, TAU0, RV, REX \\
WRITE (9, 4005) (NAVE(I), I = 1*25) \\
WRITE (9, 4022) (Y(J), J = 1*NS)
\end{align*}
\]
WRITE (10, 4011) N3, L, S, DY, TAU0, RV, RENX
WRITE (10, 4008) (NAmE(I), I=1, 25)
WRITE (10, 4022) (Y(J), J=1, NS)
900 CONTINUE

C *************** FORMAT LIST ***************
C
C 1001 FORMAT (I2, 3X, 15A3, 10A3)
C 1002 FORMAT (1HO//)
C 1003 FORMAT (1HO* 'END OF PROBLEMS. TEAR OFF THIS PAGE, GOOD LUCK."
C 1004 FORMAT (1H1)
C 1006 FORMAT (1HO* 15A3, 10A3)
C 1007 FORMAT (1HO)
C 1008 FORMAT (1HO, 'INPUT DATA (1=YES, 0=NO)'/
C 1 1 'TYPE OF CALCULATION = ', 11/
C 1 'DIMENSIONAL PSI = '', 11/
C 2 1 '0 = ', 1PE12.6/, ' RENX = ', 1PE12.6/
C 2 1 'H = ', 1PE12.6/, ' VO = ', 1PE12.6/
C 3 1 'RENY = ', 1PE12.6/, ' A = ', 1PE12.6/
C 4 1 'TAU0 = ', 1PE12.6/, 'AK = ', 1PE12.6/, 'RHO = ', 1PE12.6/
C 5 1 'S = ', 1PE12.6/, ' D = ', 1PE12.6/
C 6 1 'L = ', 15A3, 10A3/
C 7 1 'IPRT1 = '', 11/ 'INCPRT = '', 11/
C 1009 FORMAT (1HO//, '** FINAL RESULTS ** (1=II)/
C 1 1 IPRT/ 1PE12.6/ 'N = 1PE12.6/ 1PE12.6/ 1PE12.6/ 1PE12.6/
C 2 1 'TAU ***'/8(3X, 1PE12.6))
C 1010 FORMAT (1HO, '** STRFAY FUNCTION ***', 5X, 'X = ', 1PE12.6/
C 1 8(3X, 1PE12.6))
C 1011 FORMAT (1HO, '*** TAU ****/8(3X, 1PE12.6))
C 1012 FORMAT (1HO, '*** P ****/8(3X, 1PE12.6))
C 1013 FORMAT (1HO, '*** IAP ****/8(3X, 1PE12.6))
C 4008 FORMAT (1H, 15A3, 10A3)
C 4011 FORMAT (1H, 2(I3, 4X), 5(1PE12.6, 3X))
C 4021 FORMAT (1H, 1PE12.6)
C 4022 FORMAT (1H, 8(2X, 1PE12.6))
C 4044 FORMAT (1H, 4(2X, 1PE12.6))
C
C 1099 CONTINUE
C
C ******* END OF FORMAT LIST *******
C GO TO 101
C
FUNCTION FPSI(X, Y, O, H, VO, A, TAU0, AK, S, ISTYPE)
DOUBLE PRECISION FPSI, Q
C
C ******200** DECIDE TYPE OF CALCULATION *******
C
C GO TO (201, 202) ISTYPE
C
C 201 FPSI = (-5*U - VO*X)*(3 - (Y/H)**2) + Y/(2*H)
C GO TO 99
C *** 2. CASSONIAN FLUID WITH NO WALL FLUX ***

202 PF = 1.2*SORT(TAUO/H) + SORT(1.5*Q*AK**2/H**3 - .06*TAUO/H)
IF (Y .LT. 0.) Y = 0.
FPSl = (Y/A**2)*(.5*PF**2*1. - Y/H) **2/3.)*H**2
1 - 1.333333*SORT(TAUO)*H**1.5*PF*(1. - 0.4*(Y/H)**1.5)
2 + TAUO*H*(1. - .5*Y/H)>
99 RETURN
END

FUNCTION FTAU(X,Y,Q,H,V0,A,TAUO,AK,ISTYPE)
DOUBLE PRECISION Q
C ***** (0) DECIDE TYPE OF CALCULATION *****
GO TO (H01, 402) ISTYPE
C *** 1. NEWTONIAN, CONSTANT WALL FLUX ***
401 FTAU = (Q/2. - VU*X)*3.*Y*AK**2/H**3
GO TO 99
C *** 2. CASSONIAN, NO WALL FLUX ***
402 PF = 1.2*SORT(TAUO/H) + SORT(1.5*Q*AK**2/H**3 - .06*TAUO/H)
FTAlj = PF*PF*Y
99 RETURN
END

C ********** VELOCITY = PRESSURE PROGRAM **********

DOUBLE PRECISION SI
DIMENSION PSI(104,33), TAU(104,33), TAUX(104,33), VX(104,33),
1 P(104,3,), NAME(25), YR(33), XR(104)
RE = (5,4,1) ITA E
1 RE = (10,4011,END=,2) N3, L, S, DY, TAUO, RV, RENX
IF (M3 LT. 1) GO TO 99
RE = (10,4001) (Y(I,J), J=1,25)
RE = (10,4022) (Y(I,J), J=2,33)
DO 10 I = 2, L
RE = (10,4021) XR(I)
RE = (10,4041) (P:J(I,J), J=2,3)
PSI(I,J) = -PSI(I,3)
RE = (10,4022) (T U(I,J), J=2,3)
10 CONTINUE

L1 = L - 1
N2 = N3 - 1
N1 = N2 - 1
DO 20 I = 3, L1
20 JJ = J, N3
J = 2 + N3 - JJ
F2 = (PSI(I,J+1) + PSI(I-1,J+1) - PSI(I+1,J-1) - PSI(I-1,J+1))
1 /(4.*S0Y*DY)
02 = (5*5*(PS1(I,J,1) - PSI(I,J-1)) - 2.*(S5-1.)*PSI(I,J))
1 E = PSI(I,J) - PSI(I-1,J)/(S5*DY*DY)
GROUP = 4*F2*F2 + 02*02
IF (GROUP .LT. 1.E-20) GROUP = 1.E-20
TAUX(I,J) = -(TAU}/SORT(GROUP) + 2.*SORT(TAUO)*RV/GROUP**2
1 + RV.RV)*2.*F2
IF ((TAUO(I,J) .LT. TAUX(I,J)*2, LT, TAUO*TAUO) GO TO 18
VX(I,J) = (PSI(I,J,1) - PSI(I,J-1))/(2.*DY)
GO TO 19
DO 36 I = 1, M3
   TAU(I, 1:2, 1) = -TAU(I, 1:2, 1)
   TAU(I, 1:2, 2) = TAU(I, 1:2, 2) - 2 * TAU(I, 1:2, 1) - TAU(I, 1:2, 3)
   TAU(I, 1:2, 3) = TAU(I, 1:2, 3)
END DO

DO 36 J = 2, M3
   TAU(J, 1) = TAU(J, 1)
   TAU(J, 2) = TAU(J, 2) - TAU(J, 1)
   TAU(J, 3) = TAU(J, 3)
END DO

CONTINUE

GO TO 99

99 CONTINUE

90 CONTINUE

19 VX(J, 1) = VX(J, 1) + VX(J, 1)
**VELOCITY - PRESSURE PROGRAM**

```
**VELOCITY - PRESSURE PROGRAM**

DIMENSION PSI(104,33), TAU(104,33), TAUX(104,33), VX(104,33),  
1 NAME(25), VR(33), XR(104), VY(104,33)
READ (5, = 1) TAPE
1 READ (10,4011) ITAPE
IF (N3 .LT. 1) GO TO 99
READ (10,4001) (NAME(I), I=1,25)
READ (10,4021) (XR(I), J=2,N3)
DO 10 I = 2, L
READ (10,4021) XR(I)
READ (10,4044) (PSI(I,J), J=2,N3)
PSI(I,1) = - PSI(I,3)
READ (10,4022) (TAU(I,J), J=2,N3)
10 CONTINUE
LI = L - 1
N2 = N3 - 1
N1 = N2 - 1
DO 20 I = 3, 1
20 CONTINUE
00 30 I = 3, LI
VX(I,N3) = 0.
TAU(I,1) = - TAU(I,3)
TAUX(I,1) = TAUX(I,3)
TAUX(I,N3) = 0.
00 50 J = 2, N3
P(2,J) = 0.
49 CONTINUE
DO 50 I = 4, LI
DO 50 J = 2, N2
P(I,J) = P(I-1,J) - (TAUX(I,J) - TAUX(I-1,J))  
1 - (TAU(I,J+1) - TAU(I,J-1) + TAU(I-1,J+1) - TAU(I-1,J-1))  
2 *S/4.
50 CONTINUE
TAU(L,N2) = TAU(L-2,N2) - 2.*{TAU(L-2,N2) - TAU(L-1,N2)}
DO 60 I = 4, LI
P(I,N3) = P(I,N1) - (TAU(I+1,N2)-TAU(I-1,N2))/S  
1 + (TAUX(I,N3) - TAUX(I,N1))
60 CONTINUE
```
WRITE (6, 4022) (NAME(I), I=1,25)
WRITE (6, 4024) (YR(J), J=2,N3)
DO 70 I = 3, L1
WRITE (6, 4025) XR(I), (VX(I,J), J=2,N3)
WRITE (6, 4027) (VY(I,J), J=2,N3)
WRITE (6, 4026) (P(I,J), J=2,N3)
70 CONTINUE
IF (ITAPE .EQ. 0) GO TO 1
WRITE (6, 10001) N3, L, S, DY, TAU0, RV, RENX
WRITE (6, 10002) (NAME(I), I=1,25)
WRITE (6, 10003) (YR(J), J=2,N3)
DO 80 I = 3, L1
WRITE (6, 10004) XR(I)
WRITE (6, 10005) (VX(I,J), J=2,N3)
WRITE (6, 10003) (P(I,J), J=2,N3)
80 CONTINUE
GO TO 1
C **************************** FORMAT LIST *****************************
400 FORMAT (1X, 15A3, 10A3)
4011 FORMAT (1X, 2(I3, 4X), 5(1PE13.6, 3X))
4021 FORMAT (1X, 1PE13.6)
4022 FORMAT (1X, 4(2X, 1PE13.6))
4044 FORMAT (1X, 4(2X, 1PE21.14))
4023 FORMAT (1H1, 15A3, 10A3)
4024 FORMAT (1H0, "**** Y(I,J) ****/8(2X, 1PE13.6))
4025 FORMAT (1H0, "**** VX **** " = ", 1PE13.6/8(2X, 1PE13.6))
4026 FORMAT (1H0, "**** P ******/8(2X, 1PE13.6))
4027 FORMAT (1H0, "**** VY ******/8(2X, 1PE13.6))
10001 FORMAT (1H, 2(I3, 4X), 5(IPE13.6, 3X))
10002 FORMAT (1H, 2(I3, 4X), 5(IPE13.6, 3X))
10003 FORMAT (1H, 2(I3, 4X), 5(IPE13.6, 3X))
10004 FORMAT (1H, 1PE13.6)
C **************************** END OF FORMAT LIST ****************************
99 CONTINUE
END
C **************************** GPCP CONTOUR PROGRAM (1) **************************
C
DOUBLE PRECISION PSI
DIMENSION NAME(25), YR(33), PSI(104,33), TAU(104,33), XR(104)
! READ(10, 4011, END=99) N3, L, S, DY, TAU0, RV
IF (N3 .LT. 1) GO TO 99
DY = 1./N3-2
N2 = N3 - 1
READ(10, 4008) (NAME(I), I=1,25)
READ(10, 4022) (YR(J), J=2,N3)
DO 990 I = 2, L
READ(10, 4021) XR(I)
READ(10, 4044) (PSI(I,J), J=2,N3)
READ(10, 4022) (TAU(I,J), J=2,N3)
990 CONTINUE
WRITE (6, 4001) (XR(I), I=3,1)
WRITE (6, 4001) (YR(J), J=2,N3)
WRITE (11, 10099)
WRITE (11, 10001) (NAME(I), I=1,25)
WRITE (11, 10008)
WRITE (11, 10002) DY
WRITE (11,10003)
WRITE (11,10014) N2
L1 = I - 1
DO 10 J = 2, N3
WRITE (11,10004) (PSI(I,J), I=3,L1)
10 CONTINUE
WRITE (11,10005)
WRITE (11,10006)
WRITE (11,10007)
WRITE (11,10020)
WRITE (11,10021)
WRITE (11,10009)
DY = -DY
LEVT = TAU(I,N3)/8.
TLEV = LEVT
DO 20 J = 2, N3
WRITE (11,10004) (TAU(I,J), I=3,L1)
20 CONTINUE
WRITE (11,10023)
WRITE (11,10006)
WRITE (11,10024) DY
WRITE (11,10003)
WRITE (11,10014) N2
DO 30 J = 2, N3
WRITE (11,10004) (TAU(I,J), I=3,L1)
30 CONTINUE
WRITE (11,10005)
WRITE (11,10025) TLEV, TLEV, TLEV, TLEV
WRITE (11,10020)
WRITE (11,10021)
WRITE (11,10010)
WRITE (11,10026) (NAME(I), I=1,10)
WRITE (11,10011)
WRITE (11,10012)
WRITE (11,10027)
GO TO 1
4001 FORMAT (1HO, 8(3X, 1P,E12.6))
4009 FORMAT (1X, 15A3, 10A3)
4011 FORMAT (1X, 2(I3, 4X), 4(1P,E12.6, 3X))
4021 FORMAT (1X, 1P,E12.6)
4022 FORMAT (1X, 4(I2X, 1P,E12.6))
4044 FORMAT (1X, 4(2X, 1P,D22.14))
10001 FORMAT ('F', 1000.*2X, 12A3, 10A3, 2X, '15.0', 1X, '00')
10002 FORMAT ('F', 1Z, '12', 30., '0', 0.50, '2', 0.00, '1', 0.00, '5', 0.00)
     1
     1.00, 5X, '10U', 0', 5X, '0.00', 'F5.2 ', 5X, '1.00')
10003 FORMAT ('F', 1AAY, '1', 0.0, '0', 0.70, '4X', '2', '4X', '2', '3')
10004 FORMAT ('F', 1ARAY, '1', 0PE14.5, 0PF14.5, 0PE14.5, 0PE14.5)
10005 FORMAT ('F', 'RNO')
10006 FORMAT ('F', 'LEV', '2X', '0.00', '1X', '0.00', '1X', '0.50', '1X', '0.07',
     1
     2
     4
     1.00, '0.100', '0.100', '0.40', '6', '0.100', '0.40', '6')
10007 FORMAT ('F', 'LEV', '2X', '0.55', '1X', '0.55', '1X', '0.50', '1X', '0.07',
     1
     2
     4
     1.00, '0.100', '0.100', '0.40', '6', '0.100', '0.40', '6')
10008 FORMAT ('F', 'ANGL', '1', '0.00', '10.00')
10009 FORMAT ('F', 'LINE', '5X', '1', '0.00', '1.000', '1.000', '0.800',
     1
     0.07, '0.00', '5X', '3X', '2')
10010 FORMAT ('F', 'X', '5X', '0.00', '10.00', '1.000', '0.800',
     1
     0.07, '0.00', '5X', '3X', '2')
10011 FORMAT ('F', 'SYMN', '5X', '1', '0.00', '0.450', '90.00', '1X', '0.14', '4X',
     1
     3', '15X', 'PSI')
10012 FORMAT ('SYMR:', '5X:', '1:', '-10.0:', '-0.55:', '90.00:', '1X:', '0.14:', '4X:
  1
  '3:', '5X:', 'TAU')
10014 FORMAT ('ARAY:', '5X:', '1:', '2X:', '101:', '4X:', '3X:', '12)
10020 FORMAT ('PL0T')
10021 FORMAT ('PRDR')
10023 FORMAT ('HAS*)
10024 FORMAT ('SIZE*', '1X:', '12.50:', '5.000:', '2.000:', '1.000:', '5X:', '0.000^',
  1
  '1.000:', '5X:', '100:', '0.000:', 'F5.2:', '5X:', '1.000')
10025 FORMAT ('REALX*', '1X:', '2F5.2:', '1X:', 'n.50:', '1X:', '0.07^',
  1
  '2X:', '0.0:', '2X:', '0.0:', '2X:', '0.0:', '2X:', '0.0:', '4X:', '1:', '4X:',
  2
  '4X:', '2:', '2F5.2:', '3X:', '15:', '4X:', '1')
10026 FORMAT ('SYMB:', '5X:', '1:', '10.00:', ',1.50:', '90.00:', '1X:', '0.21:',
  1
  '3X:', '30:', '15X:', '10A3')
10027 FORMAT ('END*)
10099 FORMAT ('GRQT 6T*GCP,GPCP*)
99 CONTINUE
END

C ******************** PLOT (PSI)-(TAU) AT CONSTANT X *********************
C
DOUBLE PRECISION PSI
DIMENSION NAME(25), XR(104), YR(33), PSI(104,33), TAU(104,33),
  1 INUF(140)
CALL PLOT(XR(104), YR(33), PSI(104,33), TAU(104,33),
  1 INUF(140))
CALL PLOT(XR(300,0))
CALL PLOT(2.5, 5, 5, -3)
1 READ (4011, END=999) N3, L, S, DY, TAU0, RV, RENX
IF (N3.LT.1) GO TO 999
READ (4000) (NAME(I), I=1,12)
READ (4022) (YR(J), J=2,N3)
L = L - 1
DO 10 I = 2, L
  READ (4021) XR(I)
  READ (4044) (PSI(I,J), J=2,N3)
  READ (4022) (TAU(I,J), J=2,N3)
10 CONTINUE
TAU0 = TAU0 + S*DY*RV*W*
CALL PLOT(0.0, 2.5, 3)
CALL PLOT(0.0, 2.5, 2)
CALL PLOT(5.0, 2.5, 3)
CALL PLOT(5.0, 2.5, 2)
CALL PLOT(0.0, 2.5, 2)
CALL PLOT(1.0, 2.5, 3)
CALL PLOT(1.0, 2.5, 2)
CALL PLOT(2.0, 2.5, 3)
CALL PLOT(2.0, 2.4, 2)
CALL PLOT(3.0, 2.5, 3)
CALL PLOT(3.0, 2.5, 2)
CALL PLOT(4.0, 2.5, 3)
CALL PLOT(4.0, 2.4, 2)
CALL PLOT(5.0, 0.0, 3)
CALL PLOT(4.9, 0.0, 2)
CALL PLOT(4.0, 2.5, 3)
CALL PLOT(4.0, 2.4, 2)
CALL PLOT(3.0, 2.5, 3)
CALL PLOT(3.0, 2.4, 2)
CALL PLOT(2.0, 2.5, 3)
CALL PLOT(2.0, 2.4, 2)
CALL PLOT(1.0, 2.5, 3)
CALL PLOT(1.0, 2.4, 3)
CALL SYMBOL(2.2, 2.9, 0.14, 3HPSI, 0.0, 3)
CALL SYMBOL(2.2, 2.3, 1.0, 14, 3HTAU, 0.0, 3)
CALL SYMBOL(2.2, -0.9, 0.1, 14, Y, 0.0, 3)
CALL SYMBOL(0.0, -4.0, 0.21, NAME, 0.0, 3)
DO 15 J = 2, N3
   YR(J) = YR(J) * 2.5
15 CONTINUE
   DO 40 I = 2, N3
      DO 20 J = 2, N3
         PSI(I, J) = PSI(I, J) * 5.
20 CONTINUE
   DO 30 I = 2, N3
      SI = PSI(I, J)
      CALL PLOT(SI, YR(J), 2)
30 CONTINUE
   DO 50 J = 2, N3
      YR(J) = - YR(J)
50 CONTINUE
   DO 60 I = 3, LI
      PSI(I, J) = PSI(I, J) * 5.
60 CONTINUE
   DO 70 J = 2, N3
      SI = PSI(I, J)
      CALL PLOT(SI, YR(J), 2)
      IF (SI .GE. 5.) GO TO 80
70 CONTINUE
80 CONTINUE
   DO 90 J = 2, N3
      YR(J) = - YR(J)
90 CONTINUE
   DO 100 I = 3, LI
      PSI(I, J) = PSI(I, J) * 5.
100 CONTINUE
C **************************** FORMAT LIST *******************************
4001 FORMAT (1X, 12A6)
4011 FORMAT (1X, 2(I3, 4X), 5(1P12.6, 3X))
4021 FORMAT (1X, 1P12.6)
4042 FORMAT (1X, 2(I3, 1P12.6))
4044 FORMAT (1X, 4(I3, 1P12.6))
C **************************** END OF FORMAT LIST ****************************
C
C **************************** PLOT VELOCITY PROFILES ****************************
DIMENSION NAME(25), YR(33), VX(104, 33), P(104, 33), IAUF(1400),
   VP(66), YP(66), XP(104)
CALL PLOT(X(104), 1400, 2, 30, 50)
CALL PLOT():(300, 0)
CALL PLOT(1.0, 6.0, 5)
1 READ (A*4n11, END=999) N3, L, S, DY, TAUO, RV, RENX
   IF (N3 .LT. 1) GO TO 999
10 READ (A*4n08) (NAME(I), I=1, 12)
10 READ (A*4n22) (YR(J), J=2, N3)
   LI = I - 1
   DO 10 I = 3, LI
   READ (A*4n21) XR(I)
   READ (A*4n22) (VX(I, J), J=2, N3)
READ (A,4022) (P(I,J), J=2,N3)

CONTINUE
N1 = N3 - 2
N4 = N3 + 1
M2 = N1 + N3
TAU0 = TAU0 + 5*DY*RV*0.
CALL PLOT(0,0, 2,0,3)
CALL PLOT(0,0,-2,0,2)
CALL PLOT(6,0,-2,0,2)
CALL PLOT(6,0, 2,0,2)
CALL PLOT(0,0, 2,0,2)
CALL PLOT(0,0,-2,0,2)
CALL PLOT(2,0,-2,0,3)
CALL PLOT(2,0, 1,9,3)
CALL PLOT(4,0,-2,0,3)
CALL PLOT(4,0, 1,9,2)
CALL PLOT(6,0, 0,0,3)
CALL PLOT(5,9, 0,0,2)
CALL PLOT(4,0, 2,0,3)
CALL PLOT(4,0, 1,9,2)
CALL PLOT(2,0, 2,0,3)
CALL PLOT(2,0, 1,9,2)
CALL SYMBOL(2,8,-2,8,0,14,2HVX,0,0,2)
CALL SYMBOL(-9,-9,0,1,0,14,2HY,0,0,2)
CALL SYMBOL(0,2,-4,5,9,0,21,NAE,0,0,30)
DO 50 I = 3, L1, 20
DO 20 J = 2, N3
JJ = J + N3 - J
VP(J) = VX(I, JJ)*4.
YP(J) = - YR(JJ)*2.
20 CONTINUE
DO 30 J = N4, M2
JJ = J - N1
VP(J) = VX(I, JJ)*4.
YP(J) = YR(JJ)*2.
30 CONTINUE
CALL PLOT(VP(2), YP(2), 3)
DO 40 J = 3, M2
CALL PLOT(VP(J), YP(J), 2)
40 CONTINUE
50 CONTINUE
CALL PLOT(14,0,0,0,-3)
GO TO 1

C **************************** FORMAT LIST ****************************
400 FORMAT (1X, 12A6)
4011 FORMAT (1X, 2(I,3,4X), 5(1PE12.6, 3X))
4021 FORMAT (1X, 1PE12.6)
4022 FORMAT (1X, A(2X, 1PE12.6))
C **************************** END OF FORMAT LIST ****************************
999 CONTINUE
END
CALL FLOTMX(3,5, J)
CALL FLOT(1, 8, 0, -3)
1 IF (NS .LT. 1) GO TO 959
READ (6, 8) (NAME(I), I=1,12)
READ (6, 6022) (YR(I), J=2,N3)
L1 = L - 1
CO 20 I = 3, L1
READ (6, 4021) XR(I)
READ (6, 4021) (VX(I, J), J=2,N3)
READ (6, 4022) (P(I, J), J=2,N3)
CONTINUE
N1 = N3 - 2
N4 = N2 + 1
N2 = N1 + N3
TAUC = TAUO + S*DY*RV*Q*
CALL FLOT(5.0, 2.0, 3)
CALL FLOT(5.0, -2.0, 2)
CALL FLOT(6.0, 2.0, 2)
CALL FLOT(6.0, -2.0, 2)
CALL FLOT(6.0, 2.0, 2)
CALL FLOT(6.0, -2.0, 2)
CALL FLOT(0.1, 0.1, 2)
CALL FLOT(2.0, -2.0, 2)
CALL FLOT(2.0, 1.0, 2)
CALL FLOT(4.0, 2.0, 2)
CALL FLOT(4.0, -2.0, 2)
CALL FLOT(6.0, 3.0, 2)
CALL FLOT(6.0, -3.0, 2)
CALL FLOT(4.0, 2.0, 2)
CALL FLOT(4.0, -2.0, 2)
CALL FLOT(4.0, 1.0, 2)
CALL FLOT(4.0, -1.0, 2)
CALL FLOT(6.0, 1.0, 2)
CALL FLOT(6.0, -1.0, 2)
CONTINUE
DO 30 J = N2, M2
J = J - N3
VP(J) = VY(I, JJ)*1030
YP(J) = YR(I, JJ)*2.
30 CONTINUE
DO 30 J = N1, M2
VP(J) = VY(I, JJ)*1000
YP(J) = YR(I, JJ)*2.
30 CONTINUE
CALL FLOT(VF(2), YP(2), 3)
DO 40 J = 3, M2
CALL FLOT(VF(J), YP(J), 2)
40 CONTINUE
50 CONTINUE
CALL FLOT(14.6, 0.0, -3)
GO TO 1
C                                                                  C

*************** FORMAT LIST ***************
1  FORMAT (1X, 12A6)
2 FORMAT (1X, 12I3, 4X, 51PE13.6, 3X)
3 FORMAT (1X, 3PE13.6)
4 FORMAT (1X, 3PE13.6)
C                                                                  C

*************** END OF FORMAT LIST ***************
CONTINUE
CALL PLOT(14,0,3,0,999)
END

*************** PLOT PRESSURE DROP *************** P(X)

DIMENSION IBUF(i,100), NAME(25), XR(144), YR(33), VX(144,33),
1 P(104,33), PP(104)
READ (5,4001) NC1, NC2, INI, MNP
CALL PLOT(IBM(1),1400,2,30,00)
CALL PLOTX(60.01)
CALL PLOT(1.0,9.0,4-3)
CALL PLOT(0.0,-5.0,2)
CALL PLOT(8.0,-5.0,2)
CALL PLOT(8.0,0.0,2)
CALL PLOT(0.0,0.0,2)
CALL PLOT(0.0,-1.0,3)
CALL PLOT(0.0,-2.0,3)
CALL PLOT(0.1,-2.0,2)
CALL PLOT(0.0,-3.0,3)
CALL PLOT(0.1,-3.0,3)
CALL PLOT(0.1,-4.0,3)
CALL PLOT(1.6,-4.0,3)
CALL PLOT(1.6,-4.0,3)
CALL PLOT(3.2,-5.0,2)
CALL PLOT(3.2,-4.0,2)
CALL PLOT(4.6,-5.0,3)
CALL PLOT(4.6,-4.0,2)
CALL PLOT(5.4,-5.0,3)
CALL PLOT(5.4,-4.0,2)
CALL PLOT(8.0,-4.0,3)
CALL PLOT(7.9,-4.0,2)
CALL PLOT(3.0,-3.0,3)
CALL PLOT(7.0,-3.0,2)
CALL PLOT(8.0,-2.0,3)
CALL PLOT(7.9,-2.0,2)
CALL PLOT(8.0,-1.0,3)
CALL PLOT(7.9,-1.0,2)
CALL PLOT(8.0,0.0,3)
CALL PLOT(4.6,0.0,3)
CALL PLOT(4.6,-0.1,2)
CALL PLOT(4.8,0.0,3)
CALL PLOT(4.8,-0.1,2)
CALL PLOT(3.2,0.0,3)
CALL PLOT(3.2,-0.1,2)
CALL PLOT(1.6,0.0,3)
CALL PLOT(1.6,-0.1,2)
CALL SYMBOL(-0.8,-2.6,0.14,2,PF,0.0,2)
CALL SYMBOL(3.7,-2.6,0.14,3PVU,0.0,2)
CALL SYMBOL(-1.7,-7.5,0.21,2RD AXIAL PRESSURE DROP,0.0,20)
IF (NC1 .EQ. 0) GO TO 26
DO 25 K = NC1, NC2
READ (6,4011) ENDF=999, N3, L, S, DY, TAUO, RV, RENX
IF (N3 .LT. 1) GO TO 999
READ (8,4022) (NAME(J), J=1,12)
READ (8,4022) (YR(J), J=2,11)
L1 = L - 1
DO 10 I = 3, L
READ (9,4021) XR(I)
READ (8,4022) (VA(I,J), J=2,N3)
READ (9,4022) (P(I,J), J=2,N3)
10 CONTINUE
CALL PLOT(0.0,0.0,3)
DO 20 I = 4, L
P(I) = P(I,2)/300*
XR(I) = XR(I)/12.5
CALL PLOT(XR(I),P(I),2)
20 CONTINUE
YS = PP(L1)
CALL SYMBOL(10,*,YS ,0.07,NAME,0.0,30)
45 CONTINUE
46 IF (NN1 ,EQ, 0) GO TO 999
DO 50 K = NN1, NN2
READ (9,4011) (N3, L, S, D, TAU0, RV, RENX
IF (N3 ,LT. 1) GO TO 999
READ (9,4009) (NAME(I), I=1,12)
READ (9,4022) (Y(I,J), J=2,N3)
L1 = L - 1
DO 50 I = 2, L
READ (9,4021) XR(I)
READ (9,4022) (P(I,J), J=2,N3)
50 CONTINUE
CALL PLOT(0.0,0.0,3)
DASH = 1.
DO 40 I = 4, L
P(I) = P(I,2)/300*
XR(I) = XR(I)/12.5
DASH = DASH
IF (DASH ,GT. 0.) GO TO 39
CALL PLOT(XR(I),P(I),2)
GO TO 40
39 CALL PLOT(XR(I),P(I),3)
40 CONTINUE
YS = PP(L1)
CALL SYMBOL(15,*,YS ,0.07,NAME,0.0,30)
50 CONTINUE
C *************** FORMAT LIST ***************
4001 FORMAT ( )
4008 FORMAT (1X, 12A6)
4011 FORMAT (1X, 2(I3, 4X), 5(1PE12.6, 3X))
4021 FORMAT (1X, 1PE12.6)
4022 FORMAT (1X, 8(2X, 1PE12.6))
C *************** END OF FORMAT LIST ***************
999 CONTINUE
END
1 REAU (8,4611) N3, L, S, DY, TAUO, RV, RENX
IF (N3 .LT. 1) GC TO 999
READ (8,4611) (NAME(I), I=1,12)
READ (6,4921) (YR(J), J=2,N3)
L1 = L - 1
DO 10 I = 3, L1
READ (8,4921) XR(I)
READ (6,4922) (VX(I,J), J=2,N3)
READ (6,4922) (VY(I,J), J=2,N3)
READ (6,4922) (P(I,J), J=2,N3)
10 CONTINUE
M = N3 - 2
N4 = N3 + 1
M2 = M * N4
TAU0 = TAUO + S*DY*RV*0.
CALL FLOT (.C, 2.3, 3)
CALL FLOT (-.C, -2.7, 2)
CALL FLOT (-.C, -2.9, 2)
CALL FLOT (.C, 2.0, 2)
CALL FLOT (.C, 2.0, 2)
CALL FLOT (.C, 0.9, 3)
CALL FLOT (.C, 0.0, 2)
CALL FLOT (2.0, -2.9, 3)
CALL FLOT (2.3, -1.9, 2)
CALL FLOT (4.0, -2.0, 3)
CALL FLOT (4.0, -1.9, 2)
CALL FLOT (3.0, 1.0, 3)
CALL FLOT (5.0, 0.0, 2)
CALL FLOT (4.0, 2.0, 3)
CALL FLOT (4.0, 1.9, 2)
CALL FLOT (2.3, 2.3, 3)
CALL FLOT (2.0, 1.9, 2)
CALL SYMCL (2.8, -2.8, 0.0, 14, 2H, 0.0, 2)
CALL SYMCL (-2.8, -2.8, 0.0, 14, 2H, 0.0, 2)
CALL SYMCL (2.8, -2.8, 0.0, 14, 2H, 0.0, 2)
DO 50 I = 1, L1
DO 30 J = 2, N3
JJ = J + N3 - J
VP(J) = -P(I, JJ) * 4./1080.
YP(J) = -YR(JJ) * 2.
20 CONTINUE
DO 30 J = N4, M2
JJ = J - N1
VP(JJ) = -P(I, JJ) * 4./1409.
YP(JJ) = YR(JJ) * 2.
30 CONTINUE
CALL FLOT (VP(2), YP(2), 3)
DO 40 J = 3, M2
CALL FLOT (VP(J), YP(J), 2)
40 CONTINUE
50 CONTINUE
CALL FLOT (14.0, 0.0, -3)
G TO 1
C ******************************** FORMAT LIST ******************************
4036 FORMAT (LX, 12A6)
4031 FORMAT (1X, L13, 4X), 5(1PE13.6, 3X))
4021 FORMAT (1X, 1PE13.6)
4022 FORMAT (1X, 1PE13.6)
C ******************************** END OF FORMAT LIST *****************************
999 CONTINUE
CALL FLOT (14.0, 0.0, 999)
END
BIBLIOGRAPHY


VITA

Nan Wei was born on July 29, 1939, in Hupeh, China. His family moved to Taiwan in 1949. He graduated from Chien Kuo High School at Taipei, Taiwan in 1957. He received a Bachelor of Science degree in Chemical Engineering from Cheng Kung University at Tainan, Taiwan in 1961.

He received a Master of Science degree in Chemical Engineering from the Georgia Institute of Technology in 1965. He worked as a research chemical engineer with Swift and Company, Phosphate Center at Bartow, Florida from April 1965 to May 1966. Then he worked at the Research Center of United Gas Corporation in Shreveport, Louisiana from May 1966 to September 1967.

He came back to Georgia Tech in September 1967 and worked on fertilizer research projects for two and a half years before he changed to ultrafiltration work due to a shift of interest. He was employed as a research assistant or a teaching assistant most of the time during his graduate study. He was also a part-time chemical engineer with Vinings Chemical Company where he was involved in equipment design, plant design and start-up activities.

He is an associate member of AIChE and a member of ACS.